Cantera

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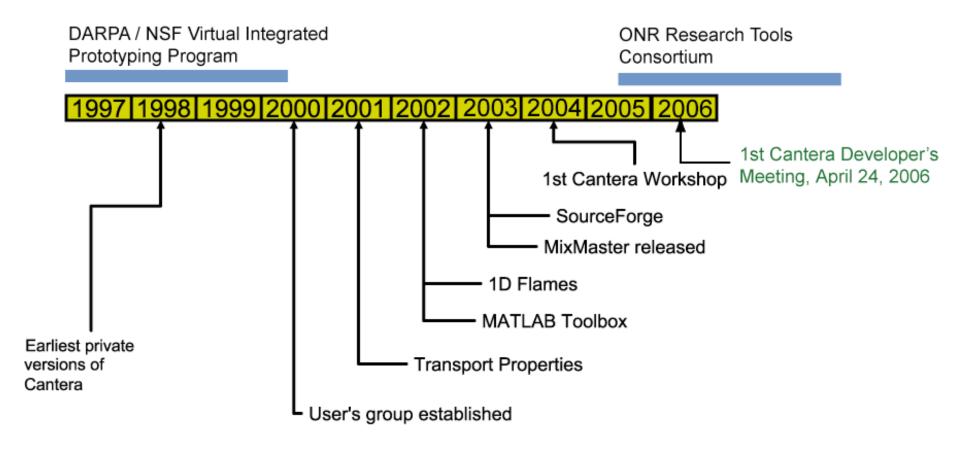
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Cantera is a suite of software tools for reacting flow problems

- Thermodynamic and transport properties
- Homogeneous and heterogeneous chemistry
- Chemical equilibrium
- Reactor networks
- Steady 1D flames
- Reaction path diagrams
- Non-ideal equations of state
- Electrochemistry

- Open source
- Object-Oriented
- Multi-Platform: Windows, Mac, linux, unix, ...
- Use from C++, Fortran 77, Fortran 90, Python, or MATLAB
- Backward compatible with CHEMKIN-II

Timeline



Cantera is designed to be easy to use, but without sacrificing performance

- Simple, intuitive structure in terms of easy-to-understand **objects**:
 - phases, mixtures, interfaces, reactors, BVP solvers, 1D reacting flows, ...
- Undergraduate and graduate student can learn Cantera and do real computations in a few hours. (Faculty take a little longer.)
 - Work in MATLAB or Python
 - no need to learn Fortran of C++
- Example scripts

- Python and MATLAB interfaces are only front ends; calculations are done in optimized, compiled code
- Cantera has most of the functionality of familiar CHEMKIN-II, plus additional capability (non-ideal phases, multiphase equilibrium, electrochemistry...)

Cantera is multilingual

 Cantera can be used from several popular programming / problemsolving environments

MATLAB Toolbox

 Interactive / scripting environments (MATLAB, Python) for rapid problem solution and software prototyping

Python Package

 Scripts can be easily translated into Fortran 90, C, or C++. **C** function library

Python interface simplifies integration with other CMDF tools

Fortran 90 module

C++ Class Library

Simple, high-level, object-oriented interface

```
>> gas = GRI30;

>> set(gas, 'T', 300.0, 'P', oneatm, 'X', 'CH4:1.0, O2::2, N2:3.76'););

>> equilibrate(gas,'HP');

>> temperature(gas)

ans =

2.220222916787240e+03
```

Multiphase equilibrium is also easily formulated and solved

```
4.5
from Cantera import *
                                                        3.5
phases = importPhases('KOH.cti',
              ['K_solid',
                                                         3
               'K_liquid', 'KOH_a', 'KOH_b',
                                                        2.5
               'KOH_liquid', 'K2O2_solid',
                                                         2
               'K2O solid', 'KO2 solid',
                                                        1.5
               'ice', 'liquid water', 'KOH plasma'])
mix = Mixture(phases)
                                                        0.5
f = open('equil_koh.csv','w')
                                                           0
                                                                   1000
                                                                            2000
                                                                                     3000
                                                                                               4000
                                                                                                        5000
writeCSV(f,['T']+mix.speciesNames())
for n in range(500):
  t = 350.0 + 10.0*n
  mix.set(T= t, P = OneAtm, Moles="K:1.03, H2:2.12,
     O2:0.9")
  mix.equilibrate("TP",maxsteps=1000,loglevel=0)
  writeCSV(f,[t]+ list(mix.speciesMoles()))
```

f.close()

K(cr)

K(L)

KOH(a) KOH(b) KOH(L)

K2O2(s) K2O(s)

KO2(s)

H2O(s)

H2O(L)

Electron

H+

HO2 H2

H2+ H2-H2O

H2O+

6000

Cantera has a similar 'look and feel' in all environments

MATLAB

```
gas = importPhase('gri30.cti');
setState_TPX(gas,300.0,OneAtm,'CH4:1,O2:2,N2:7.52');
equilibrate(gas,'HP');
disp(gas)
```

Python

Fortran 90

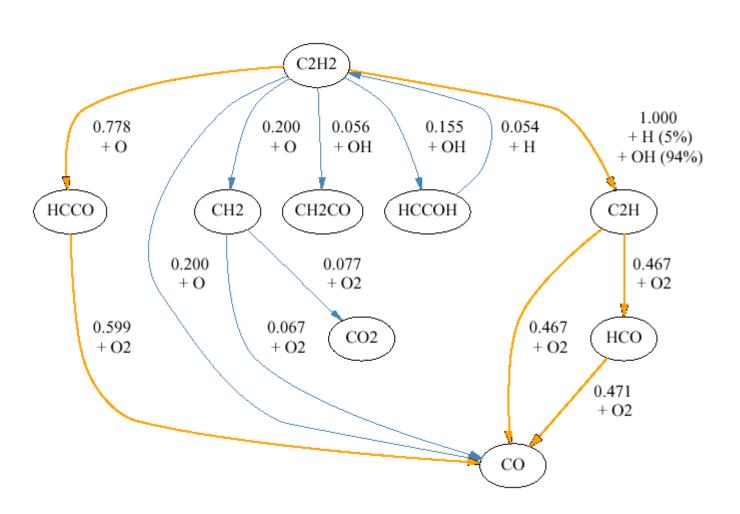
```
program equil
use cantera

type(gas_t) gas
gas = IdealGasMix('gri30.inp')
call setState_TPX(gas, 300.0,OneAtm,'CH4:1,O2:2,N2:7.52')
call equilibrate(gas,'HP')
call printSummary(gas)
end
```

```
from Cantera import *
gas = importPhase('gri30.cti')
gas.setState_TPX(300.0,OneAtm,'CH4:1,O2:2,N2:7.52')
gas.equilibrate('HP')
print gas
```

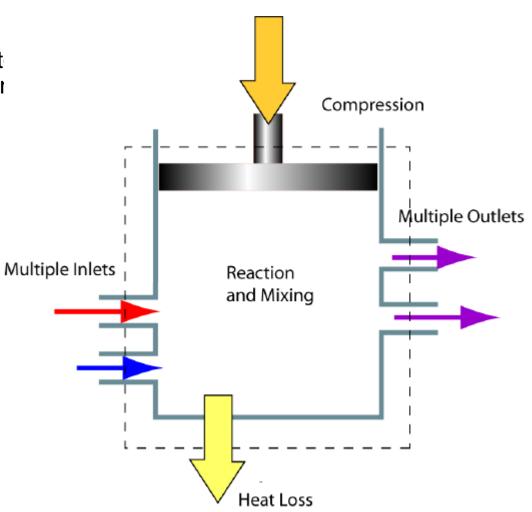
Reaction Path Analysis

Reaction path diagrams can be generated at any point in a simulation

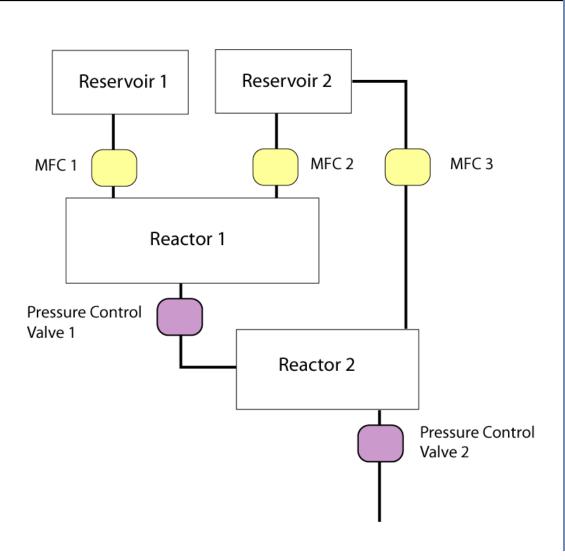


Stirred Reactor Models

- Generic transient stirred reactor model can be used to build many different batch are continuous reactors
- Mass flow rates, heat loss, volume change may all be varied as functions of time
- Reactors can be linked to create complex process models with sensors and closed-loop control



Reactors may be connected in arbitrary networks



Reservoirs provide specified inputs

Each reactor may use a different mixture model or reaction mechanism

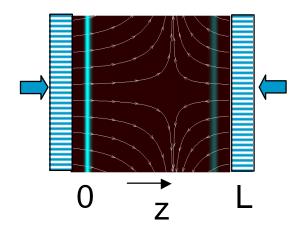
Flow control devices with closed-loop (PID) controllers

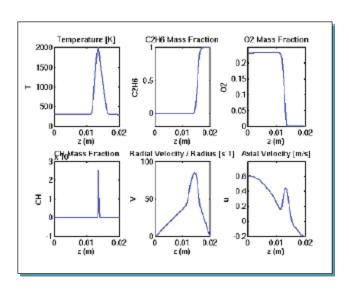
Can assemble many different processes from a small set of components

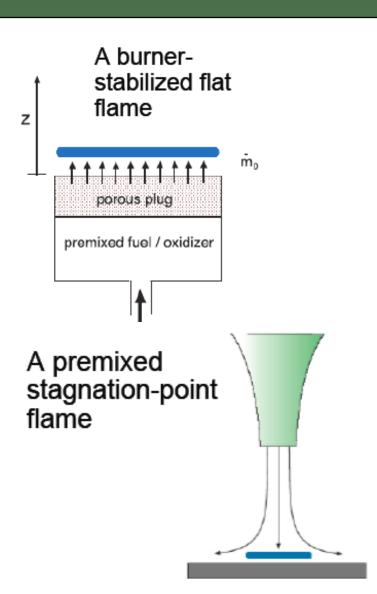
All inputs may be timedependent

One-Dimensional Flames

Conterflow premixed or non-premixed flames

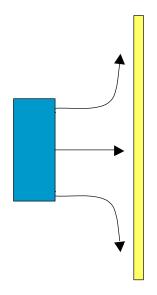


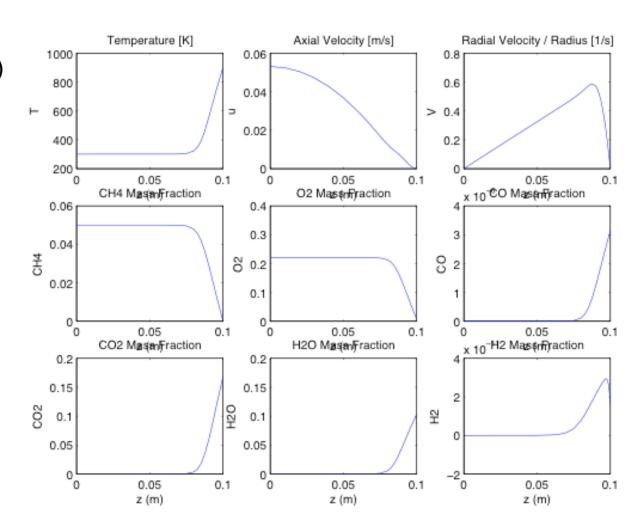




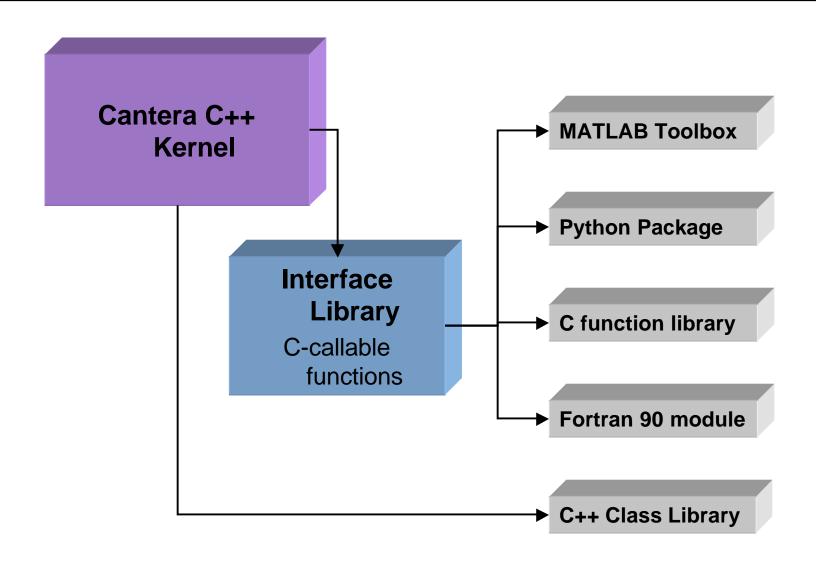
Catalytic Combustion

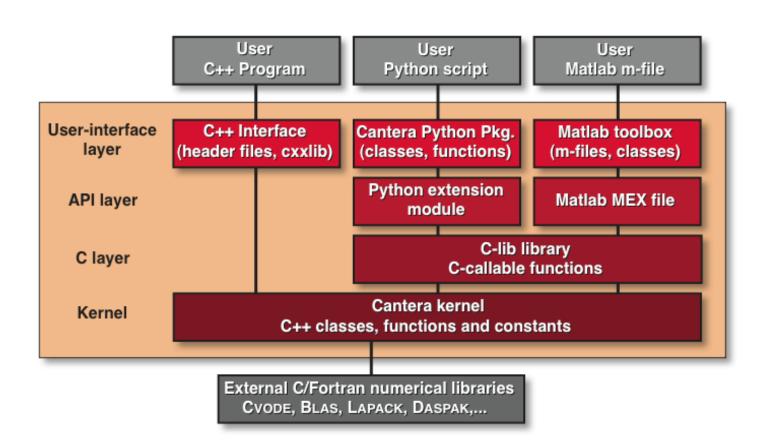
- Mechanism of Deutschmann (1995)
- 9.5% methane in air
- Platinum surface
- Tin = 300 K
- Tsurface = 900 K
- 10 cm separation





All interfaces use a common C++ kernel





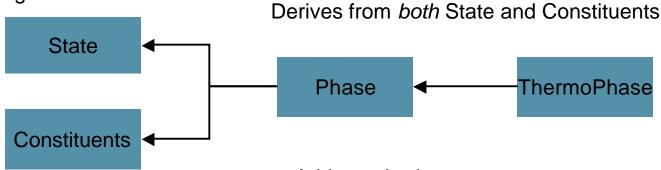
The Kernel

- C++ class library
- Designed for efficiency
 - Property caching
 - Virtual methods used sparingly
 - Templates used to allow inlining at compile time
 - Standard Template Library container classes used
 - CPU-intensive code hand-optimized
- Uses standard open-source numerical libraries
 - BLAS, LAPACK, CVODE

class hierarchy for all phase types (gases, solids, surface phases, ...)

Begin with a simple class that only knows thermodynamic **state** data (T, ρ, mass fractions) + molecular weights

Adds "placeholder" virtual functions for thermo properties. Defines the iinterface for concrete classes representing specific phase types.



Adds methods to

- save/restore state
- specify composition using strings:

"CH4:1.0, O2:2.1, N2:3.76"

Attributes of **constituent** elements and species (name, mass, Wheat Garalited Proposition,

charge get/set temperature and density

- get/set mass and mole fractions
 Still no thermo properties (other than temperature
- compute useful functions of composition). These require knowledge of EOS.

Chemkin-II compatibility

- Converter for Chemkin mechanism files into Cantera CTI format
- Thermodynamic, kinetic, and transport models implemented in Chemkin-II are also implemented in Cantera (and others not in Chemkin-II)
- Very straightforward to write a Fortran-callable library with same interface as the Chemkin-II libraries, allowing easy porting of existing applications

Example: A Cantera look-alike for the Chemkin-II library subroutine CKWYP

```
subroutine ctwyp(p,t,y,ickwrk,rckwrk,wdot)
      implicit double precision (a-h,o-z)
      double precision y(*), rckwrk(*), wdot(*)
      integer ickwrk(*)
                                                       convert cgs to SI units
      set the state
C
      psi = 0.1*p
      call setState_TPY(t, psi, y)
                                                       set the state using T, P, Y
      get the net production rates
C
      call getNetProductionRates(wdot)
                                                       compute the production rates
      convert SI -> cgs
C
      nsp = nSpecies()
      do k = 1, nsp
         wdot(k) = 1.0d3*wdot(k)
                                                       convert results from SI to cgs
      end do
                                                       and return
      return
      end
```

Current Status

- Web-based user's group with nearly 500 members
- Membership still growing rapidly
- 15 20 downloads from Sourceforge per day
- Used in combustion courses at Caltech, Berkeley, Stanford, ...
- Likely that Cantera will be used in the next version of Fluent for property evaluation, kinetic rates, and chemical equilibrium
- Interest at Sandia in porting some very large reacting flow codes to Cantera

Where to from here?

- Current capabilities are adequate for many users
- New capabilities on the horizon
 - Electrochemistry (fuel cells, corrosion)
 - Equations of state for ionic liquids (Debye-Huckel)
 - A sectional aerosol model with surface chemistry
- Current development model must change
 - Changes / enhancements to the code must consider impact on all users
 - Mechanism needed to propose, discuss, and implement changes
- Providing support for a growing user community is becoming an issue

A Diverse User Community

Users

- Students, combustion researchers, engineers
- May be familiar with engineering tools like MATLAB
- Don't know (or want to learn) C++
- Relatively small calculations

User Requirements

- "hand holding" to install software on PC
- foolproof binary installers
- support for Windows OS
- interfaces for MATLAB and scripting languages
- a simple, intuitive user interface

Developers / power users

- require access to source code
- unix-like (linux/Mac) OS
- want to call from their own codes
- large-scale simulation

Developer Requirements

- efficient libraries
- call from C++, C, and/or Fortran
- documented source code

Standards

- Cantera should be able to make use of other tools being developed elsewhere
- For example (hypothetical!) a user could type in Python

```
fullmech = getBestModel(src = 'Prime', type='CH4/air flame', ...)
reduced_mech = fullmech.reduce(method = 'RIOT', max_species = 10, ...)
```

- Not hard to do. Python has capabilities to send/receive data over the web, including filling out web forms
- Would be better, however, if XML standards existed to mediate the exchange of data