Belanak FPSO – 5 years of Successful Operation and Its Application to Floating LNG Conc

ConocoPhillips

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belanak

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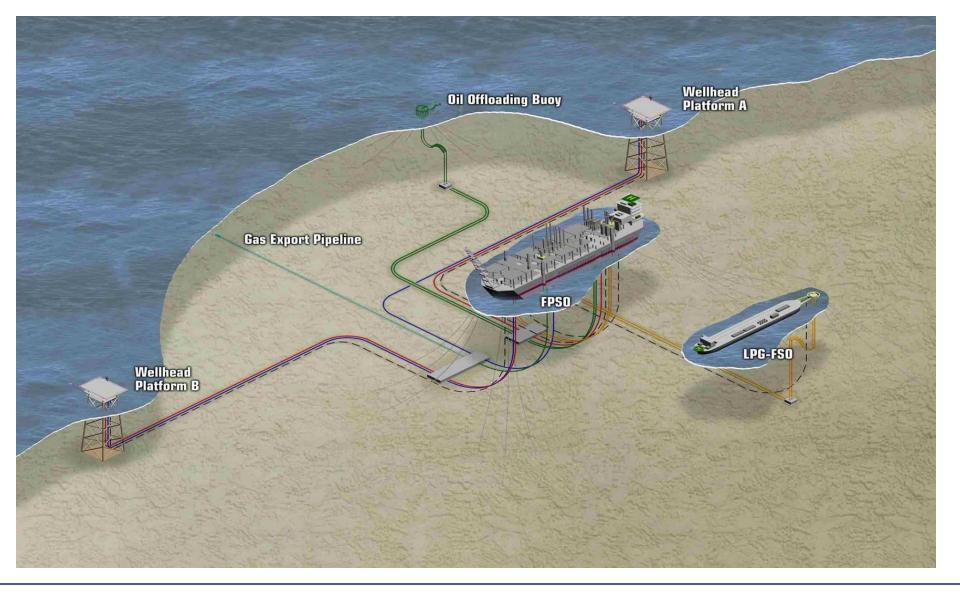
- 1. Block B Indonesia
- 2. Field Development
- 3. FPSO Project
- 4. FPSO Operating Experience
- 5. Optimized Cascade[®] Process Overview
- 6. Floating LNG Challenges
- 7. Stepping Stones to FLNG

Optimized Cascade[®] is a registered trademark of ConocoPhillips Company

COP Integrated Gas – SE Asia



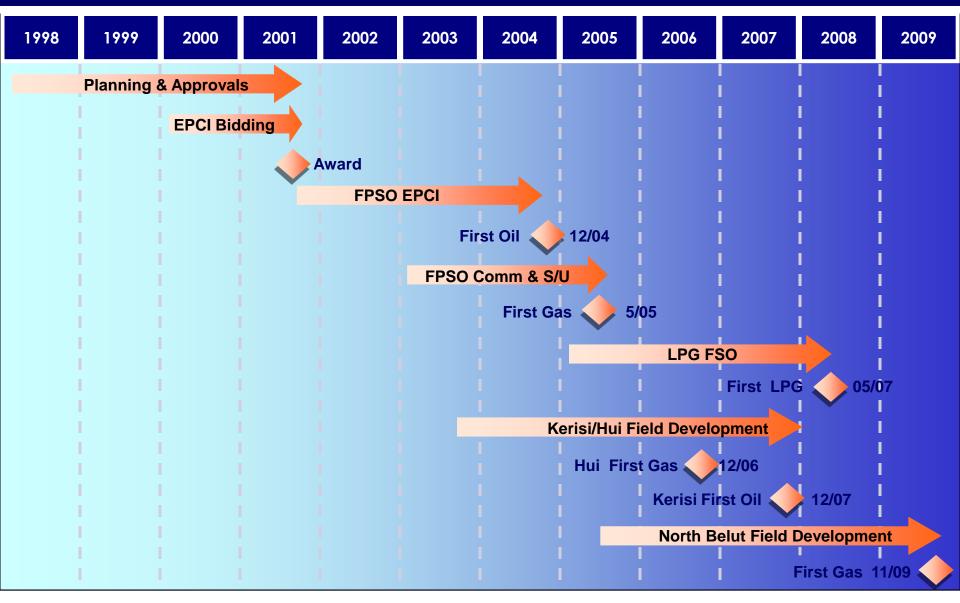
Belanak Field Development Plan



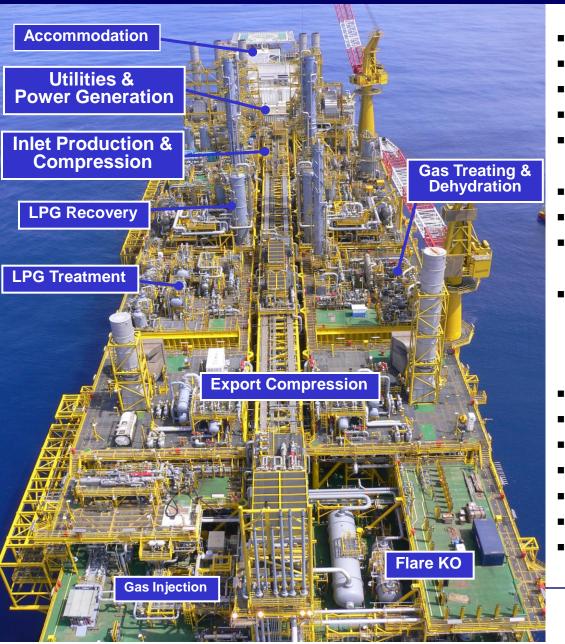
19 FPSO MODULES (~25,000 Te)



Eastern Hub Development



Belanak – Some Facts

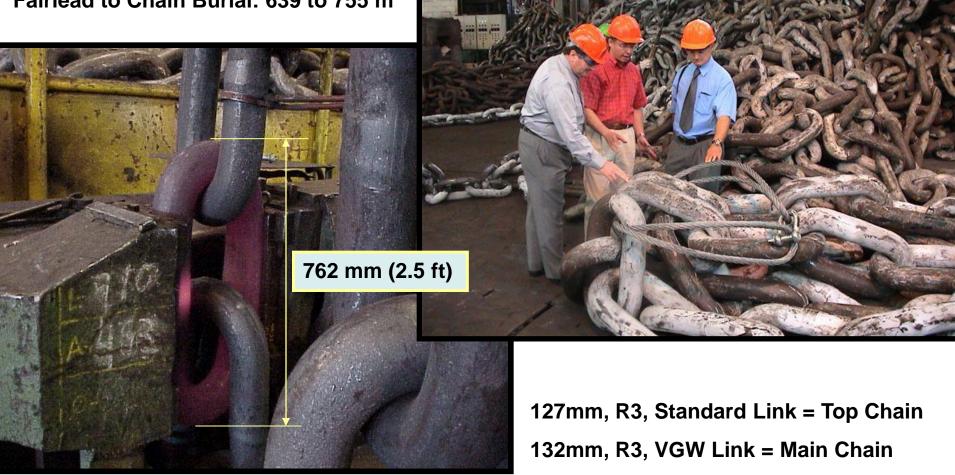


- 100,000 BPD Oil
- 500 MMSCFD Produced Gas
- 25,000 BPD LPG
- 4,000 BPD Condensate
- 120 Person Living Quarters
 - 285m LOA x 58m W x 26m D
 - 1,140,000 Bbls oil storage
- 11 km of anchor chains
- 112 MW of gas turbines
 - 2 x RR RB-211 Export Compression
 - 5 x RR Avon Power Generation
- 25,000 Te of topsides (dry)
- 7,500 Te of structural steel
- 225 pieces of equipment
- 2,500 valves
- 34 km of piping
- 117 km of cable
- 3,500 peak construction labor

FPSO Fixed Mooring System

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14 Suction Piled Anchor Chains Total Length: 10,750 m Max pull: 358 Te (398 Te 2 stall) Fairlead to Chain Burial: 639 to 755 m





High Pour Point Waxy Crude

- Wax Appearance Temperature as high as 55 °C
- Pour Point as high as 24 °C
- Mercury content

Blending with gas plant condensate reduces WAT for offloading Mercury contamination managed through testing and process optimization

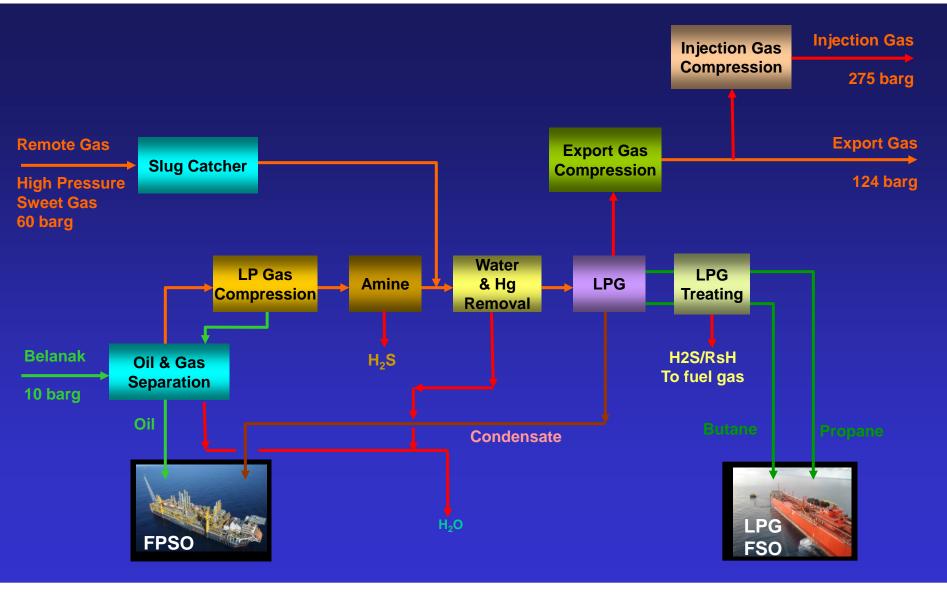
Sour Gas

- Up to 100 ppm H2S
- 8-10% CO2
- Mercaptans
- Mercury

Gas treatment to pipeline specification

Mercury Guard bed and Hg Sieve adsorbent in the Molecular Sieve for series mercury removal and polishing upstream of aluminum feed gas exchangers

Belanak Topsides Process Flow



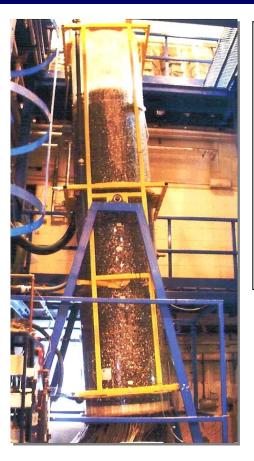


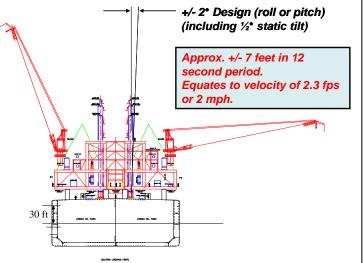
- Ship Motions Impact on Distillation
- Safety of LPG Inventories
- Commissioning & Start-Up

The Voyage to Floating LNG – Belanak

- Gas treatment & processing design for vessel motions

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Process Column Design Limits

- +/- 2° roll or pitch
- Roll/pitch/trim exceeds 1.75° < 1%

Design Approach

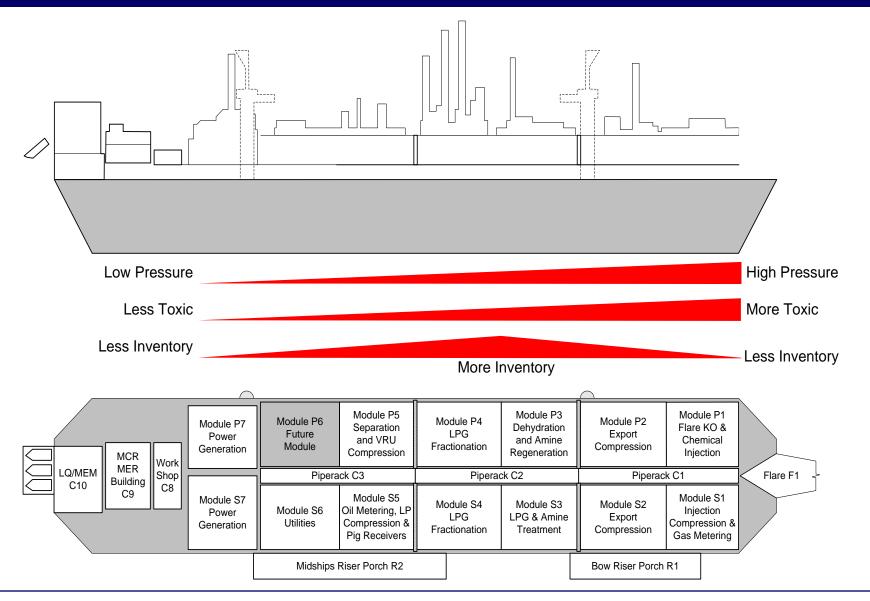
- Only use proven distributor design
- Extensive design verification
- Close inspection
- Motion distributor testing at supplier

Packing Motion Tests

- Random & Structured packing
- Distribution is critical to performance

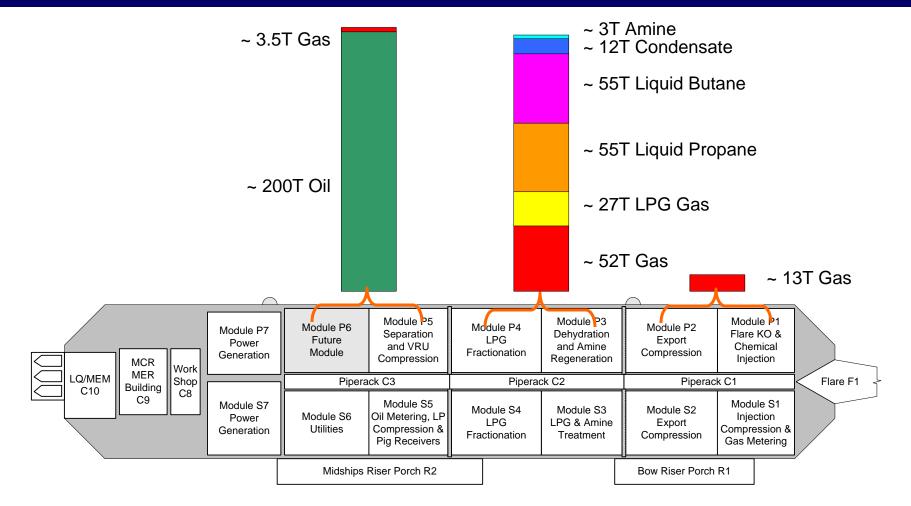
Belanak FPSO Topsides Layout





Topsides Hydrocarbon Inventory





The Belanak FPSO topsides contains ~ 415 Tonnes of Gas or Liquefied Gas



Design Phase Activities

- Maximise Inherent Safety
- Risk Based Design (Safety Case Approach)
- Formal HSE Assessment Process
 - Identify
 - Assess
 - Mitigate
- Implement Risk Reduction Measures
- Design verification (quality of engineering)
- Ease of Operability and Maintainability
- Quality control (materials, equipment, construction)

Overall Aim – Consider all Eventualities and Achieve Zero Design Defects

Belanak FPSO – Integration

Gas Plant Module Lift (S4) 2,347 Te Lift Weight Asian Hercules II in Batam Island Indonesia



Belanak FPSO – Module S4 Lift



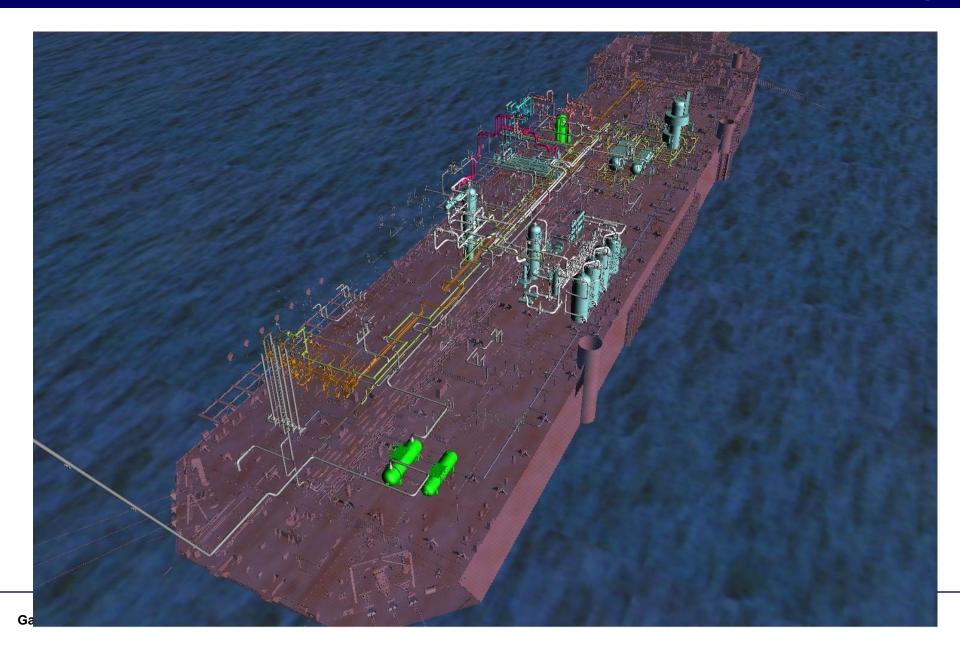
Belanak Startup HSE Readiness Plan

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HSE Start-up Readiness Plan covers 15 elements of the COPI HSE Management System

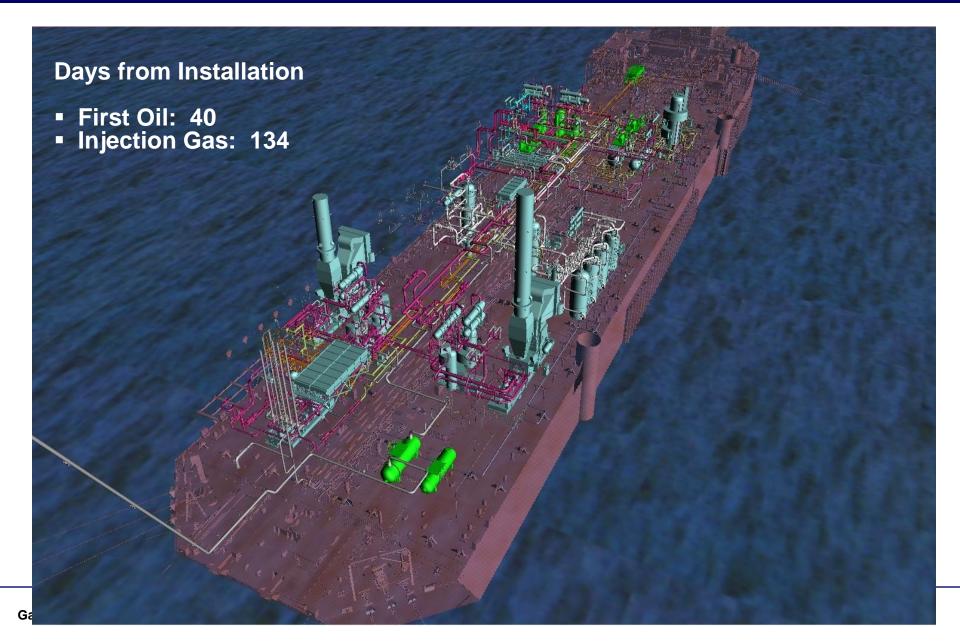
- Management's commitment towards HSE
- Operational risk assessment & management process
- Maintaining compliance with Legal requirements and operating standards
- Establishment of HSE strategies & planning
- Establishment of HSE structure and roles/responsibilities
- Development of Belanak HSE site-specific procedures/programs
- Managing changes to organization and personnel
- Managing emergency preparedness
- Delivery of mandatory HSE training
- Managing Non-conformance & corrective action process
- Development of HSE communication system
- Managing HSE document control process/system
- Managing HSE Performance measurement & monitoring
- Development of HSE Audit/inspection system
- Managing HSE Review

Phase 1 Start-up: First Oil – Dec 3 2004



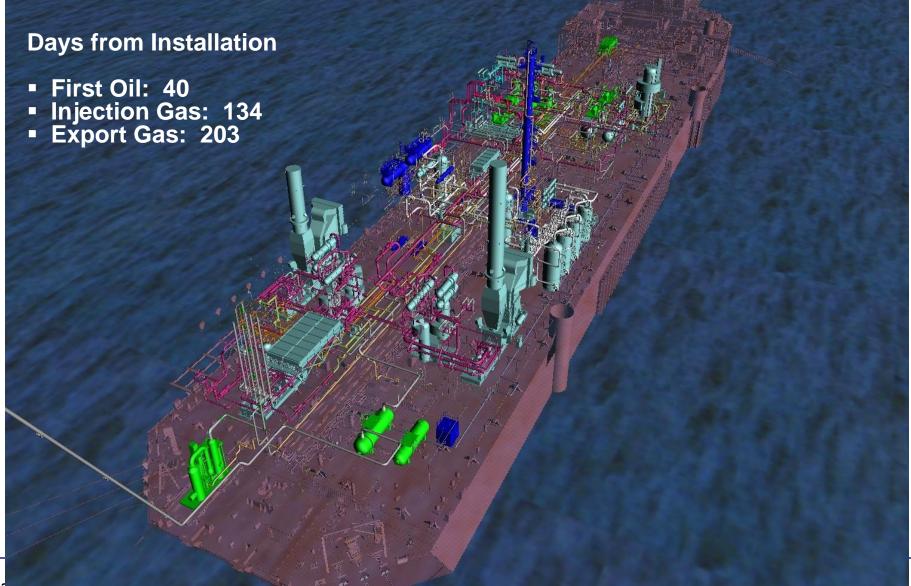
Phase 2 Start-up: Injection Gas 7 March 2005



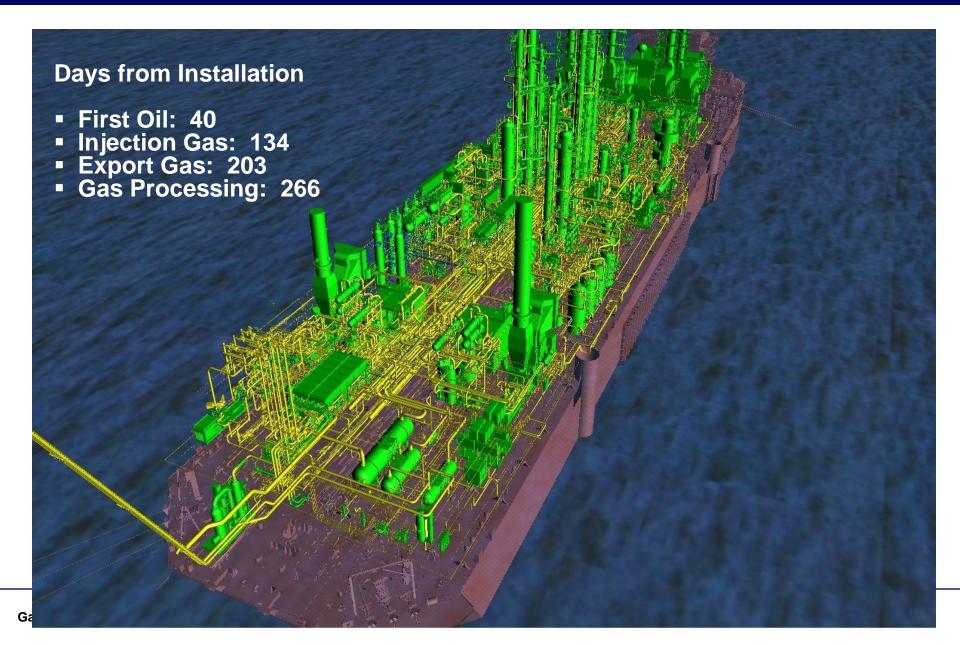


Phase 3 Start-up: Export Gas May 15, 2005





Phase 4 Start-up: Gas Processing July 17, 2005 ConocoPhillips



FPSO Start-Up Lessons Learned



- Early planning of offshore activities and utilizing a phased offshore start-up approach allowed for flexibility in start-up
- Water circulation through oil systems proved isolation and control system in preparation for first oil
- Dynamic simulation / Operator Training Simulation assisted engineers and operators prepare for start-up operations
- Integrated "One Team" approach between project and operations led to a more efficient handover and management of simultaneous operation activities
- Commissioning scope growth offshore. Need a more robust assessment of carryover prior to sail away

World Class Project Safety Performance ConocoPhillips

- Hull Fabrication: 4,200,000 man-hours Zero LTI
- Hull Tow Zero LTI
- Offshore Installation: Zero LTI
- Over 8,500,000 man-hours at topsides fabrication and integration site with only one LTI
- Project TRR of 0.374 (per 200,000 hrs)

Belanak Operations (2005 – 2010)

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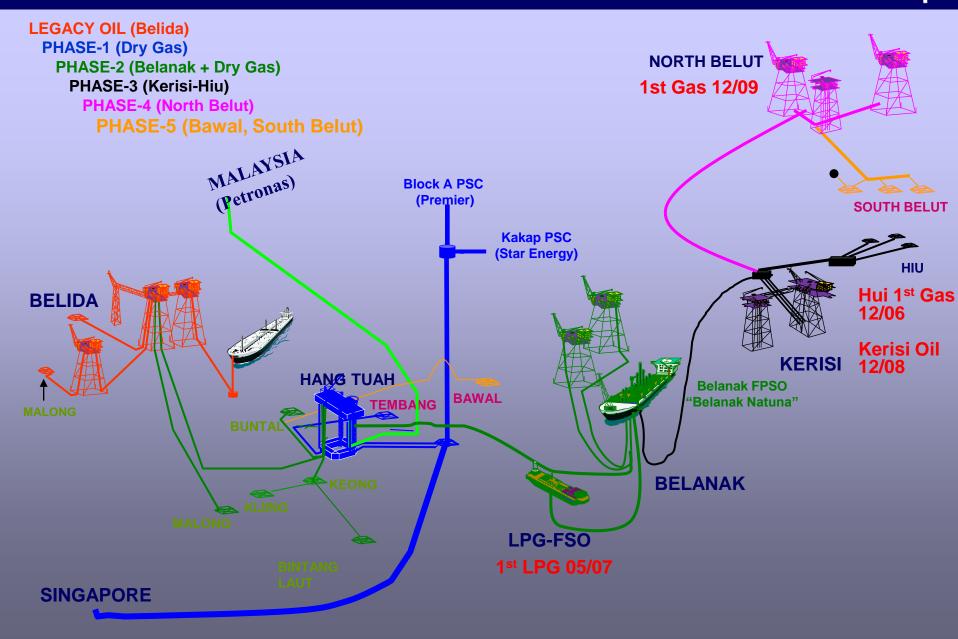
2,000+ DAYS OF SAFE OPERATION (Zero LTI)

4,000,000+ Man-hours in over Five Years of Operation

Last Recordable Incident was 19 Jul, 2005 (LTI during initial Start-up Operations)

FRATING W

Offshore Block B Development

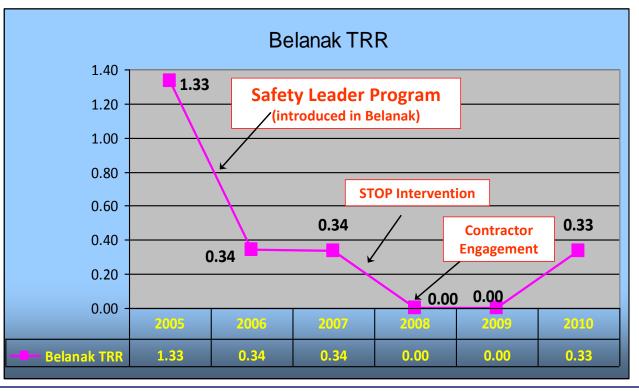


Belanak Operations Safety Statistics

- Normal Operations Crew Size of 120 person
- 4,000,000+ Operational Man-hours
- July 19th, 2010 milestone of 5 years without LTI

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Currently 2,000+ days since last LTI



Belanak Operations HSE Program

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In Operations, the Belanak Team Incorporates Safety into all Activities

- Focus on Leading Safety Metrics:
 - STOP Program
 - HSE Audits (Self Assessment, BU & Corporate)
 - Risk Assessment & Hazard Identification
 - Safety Campaigns
 - Near Miss Analysis

 - Contractor Engagement Occupational Health Programs
 - Industrial Hygiene Programs
 - Health Challenge Programs
 - **Environmental Performance Monitoring**

Apply Lessons from Trailing Metrics: Increasing Consecut

- TRR
- HSE Snapshots
- Safety Milestones
- Incident Pyramids
- **Incident Analysis**

SHOW THAT YOU CARE FOR EACH OTHER REPORT NEAR-MISS!

INY NEAR-MISS MAY NOT BE AS

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GasTech Amsterdam, March 2011

Personal Safety 30

atality

Significant

Demand on

Safety Syster

Safe Operati Envelope Excee

Process

Lost Time

Recordable

First Aid Case

afety Near Miss

Belanak FPSO Reliability

- Belanak production availability exceeded 94% in 2010
- Operability Assurance program permits flexibility in operations
- Operations Excellence program drives high availability
 - Integrated Planning & Scheduling
 - Opportunity Maintenance Optimization
 - Maintenance & Reliability System
 - Production Surveillance & Optimization System
 - Asset & Operating Integrity Management
 - Ongoing Minor Capital Improvement Program

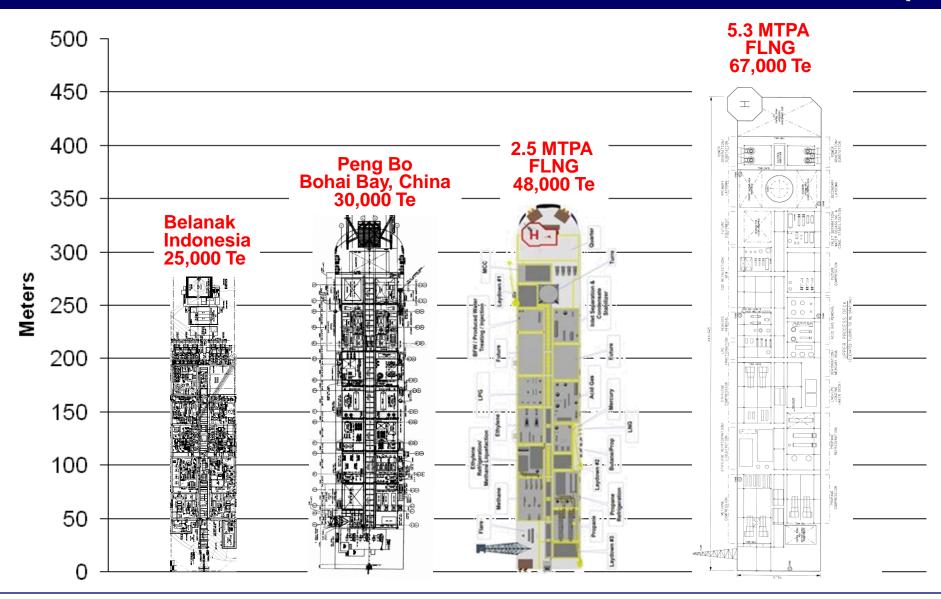




FPSO Production Availability

Belanak FPSO Production Availability 100% 98.2% 97.8% 98.0% 96.9% 97.7% 97.4% 95.4% 94.3% 92.6% 92.4% 91.9% 92.0% 91.8% 89.0% 90% 87.5% 80% 70% Direct Operating Efficiency 60% 50% 40% 30% 20% 10% 0% 2008 2009 Feb Jul Sep Oct Dec 2010 Apr Aug Jan Mar. May Jun Nov

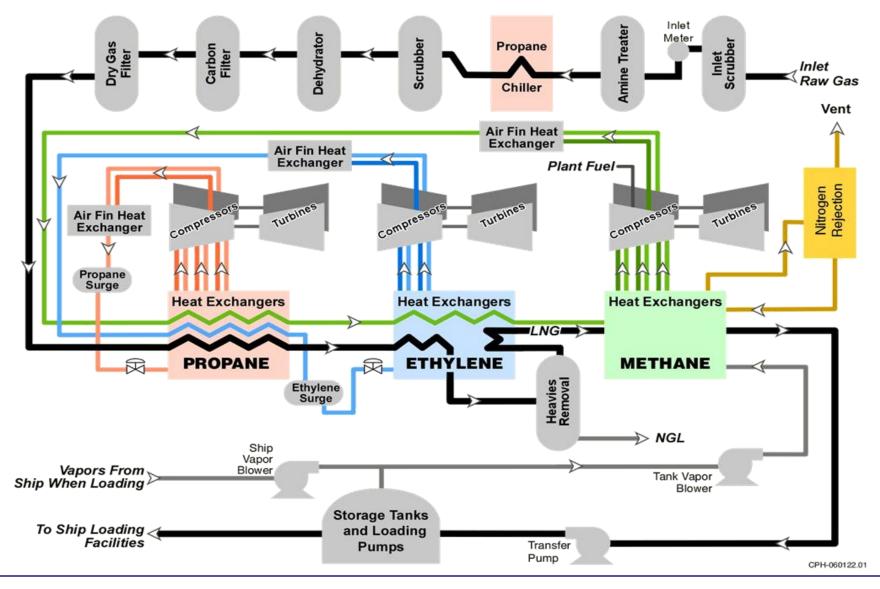
From Belanak to FLNG Hull & Topsides





- Vessel Motion impact on process equipment
- Process Hazard Mitigation
- Unsteady production flow (closer to production system)

The Optimized Cascade Process



Optimized Cascade – Advantages for FLNG

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Proven Process

Ease of Operation

- Two-Trains-in-one Reliability
- Pure Refrigerants

Direct Drive Aeroderivatives

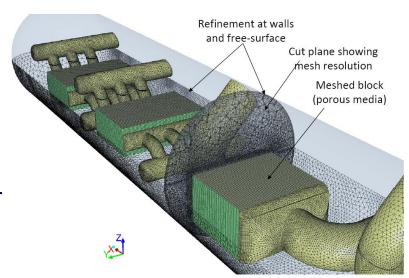
- Used Successfully at Darwin LNG
- Light Weight and Rapid Replacemer
- FPSO Experience
- Efficient

Cold Box Design

- Low Profile Exchangers Well Suited for Marine Environment
- Tall Vessels Limited to Fractionation and Amine Columns
- Modular Construction

Flexible Regarding Sudden Changes in Gas Rate

Operability, Turndown and Simplicity



Minimizing Risk



Mitigating Risk through Design and Layout

- Cryogenic Spills:
 - Cold Box Design
 - Protective Coating
- Fire & Gas Explosion
 - Layout Mitigation
 - Isolation, Relief & Blowdown Philosophies
 - Alternative Refrigerants to replace hydrocarbon based refrigerants
- Tank Dome Fire Protection
 - Lower Process Decks Plated And
 - Passive Fire Protection Applied
- Accommodation Protection:
 - Separation Via Blast Wall, Fire Wall and Layout Principles
 - Location up wind from process
- Low-speed Collisions: Double Hull Design Includes Collision Bulkheads and Fendering Plans



- Continue Developing Integrated FLNG Solutions
- Safety Risks Reduction Measures
- Key Component Designs for Motion
- Perform Full QRA on a mid-scale 2 to 3 MTPA design
- Review Marine Technology Developments
- Refine the EPC Philosophy, Execution Plan and Cost
- Field Specific Pre-FEED Study in 2011
- Prepare to implement in 2016-2019 timeframe