

### FRANCISCO JOSEPHINUM WIESELBURG

## BIOMASS I LOGISTICS I TECHNOLOGY



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Pellet burner PELLEMATIC PE32

### Applicant and manufacturer:

ÖkoFEN Forschungs- und Entwicklungs Ges.m.b.H. Mühlgasse 9 4132 Lembach i. M., Austria



The BLT Wieselburg is an accredited burner test centre issued with identification number 112 according to accreditation law BGBI. no. 468/1992. The quality management system is compliant with the requirements of ÖVE/ÖNORM EN ISOIEC 17 025.



### FRANCISCO JOSEPHINUM WIESELBURG

## BLT - BIOMASS I LOGISTICS I TECHNOLOGY

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The test results detailed in this test report exclusively refer to the test piece specified in the chapter "Boiler plate information".

The test report must be published only literally and unabridged. Exceptions must be authorized by FJ-BLT.

Authorized translation
In the event of doubt, the German original shall prevail

## **TABLE OF CONTENTS**

				Page
1	DES	CRIPT	ION	1
	1.1	Gener	al	1
	1.2		plate information	
	1.3	Diagra	am of the burner	2
	1.4	Techn	ical data	2
2	TES	TS AN	D RESULTS	3
	2.1	Test s	etup – measurement methods	3
	2.2	Perfor	mance of heating tests	4
	2.3	Interp	retation of emission measurements	4
	2.4	Invest	igatory heating tests with wood pellets at nominal heat output	5
		2.4.1	Emission measurements	6
		2.4.2	Evaluation	6
		2.4.3	Output-related measurements	
		2.4.4	Flue gas composition	
	2.5		igatory heating tests with wood pellets at minimum heat output	
		2.5.1	Emission measurements	
		2.5.2	Evaluation	_
		2.5.3	Output-related measurements	
		2.5.4	Flue gas composition	
	2.6		ce losses	
	2.7		-side resistance of boiler	
	2.8		ical power consumption	14
		2.8.1	Average electrical power consumption at nominal heat output, minimum heat output, during standby position and ignition	1.1
		2.8.2	Electrical power consumption of main loads	
_			·	
3			OF RESULTS	
	3.1		ng tests	
	3.2		on check of the temperature controller / safety temperature limiter on the boiler	
	3.3	Functi	on check to verify the rapid shutdown of the burner system	16
4	ASS	ESSM	ENT	16
5	APP	ENDIX		17
	5.1		requirements (for information only)	
	5.2	Surfac	ce temperature measurement points	18



## **APPLIED STANDARDS**

[1]	ÖNORM EN 303-5:1999	Heating boilers for solid fuels, hand and automatically stoked, nominal heat output of up to 300 kW.
[2]	ÖNORM EN 304:1992/A1:1998	Heating boilers. Test code for heating boilers for atomising oil burners
[3]	EN 267:1999	Forced draught oil burners - Definitions, requirements, testing, marking
[4]	ÖNORM M 7135:2000	Compressed wood and compressed bark in natural state - Pellets and briquettes - Requirements and test specifications
[5]	DIN 4702-1:1990	Central heating boilers - Terms, requirements, testing, marking
[6]	DIN 4702-2:1990	Central heating boilers - Test code

#### 1 DESCRIPTION

#### 1.1 General

The tested pellet burner PELLEMATIC PE32 manufactured by ÖkoFEN Forschungs- und Entwicklungs Ges.m.b.H. with a nominal heat output of 32.0 kW comprises a storage container, a fuel feeding system with integrated fire protection valve, the burner including burner plate, the flame pipe and the attached pipe heat exchanger with cleaning springs. The burner is equipped with electric ignition, an automatic cleaning system for the heat exchanger, a speed-controlled combustion fan and a microprocessor control system with associated switches and sensors.

A sheet metal storage container was used to perform the tests. An extraction screw transports the fuel through the entry pipe with integrated burn-back ball valve to the stoker screw. The stoker screw is driven by a gear motor and transports the fuel from below onto the heat-resistant steel burner plate. The fuel is ignited by an electric heating cartridge. The burner is regulated by a system using a combustion fan, the boiler temperature sensor and the combustion chamber temperature and pressure sensors to control the heat output. A radial fan directs the combustion air as the primary air flow through the fuel and as a secondary air flow to the fuel gas via a post-combustion ring in the flame pipe. The combustion gases then exit the flame pipe and flow into the heat exchanger. The heat exchanger is automatically cleaned by internal cleaning springs actuated by a motor. The ash from the heat exchanger and burner is collected in an ash drawer below the burner plate. The combustion chamber and heat exchanger are thermally insulated from the outside.

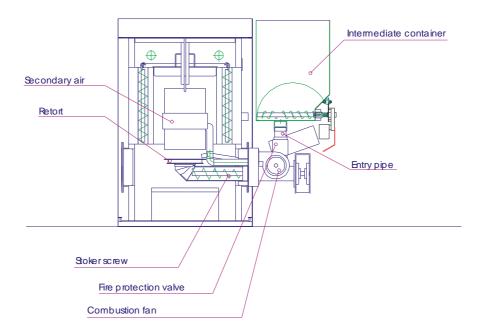
The ignition process is monitored by measuring the combustion chamber temperature. Once ignition has been successful, the control system switches to heating mode and controls the heat output level according to the required heat output. The fuel and combustion air quantities are preset for various heat output levels and then regulated during operation according to the boiler temperature and combustion chamber temperature.

#### 1.2 Boiler plate information





# 1.3 Diagram of the burner



#### 1.4 Technical data

Parameter – Overall dimensions of burner	Value	Unit
Overall length including burner and intermediate container	1200	mm
Overall depth including flue gas pipe connection	1160	mm
Overall height	1335	mm
Diameter of flue gas pipe	150	mm
Height to centre of flue gas pipe	480	mm
Flow/return connection	5/4	"
Water capacity	101	I
Emptying outlet	1/2	"
Thickness of sheets exposed to fire (stainless steel)	2	mm
Thermal insulation	40 – 100	mm
Total weight (boiler + burner + storage container)	493	kg

Source: Measurements by BLT Wieselburg

Parameter – Storage container (testbed)	Value	Unit
Container diameter	390	mm
Container height	740	mm

Source: Measurements by BLT Wieselburg



#### 2 TESTS AND RESULTS

Measurements were taken to determine the heat output, boiler efficiency (direct method), flue gas composition, flue gas temperature in the measuring section, feed pressure (draught), emission characteristics and electrical power consumption. The surface temperatures were measured at nominal heat output and stationary operation; this allowed the surface losses to be estimated.

The measurement equipment and measurement method correspond to ÖNORM EN 303-5:1999, ÖNORM EN 304:1992/A1:1998 and EN 267:1999. The measurement accuracy and measurement uncertainty are stated in documented procedures for verification in the quality management manual issued by the Federal Institute of Agricultural Engineering (Bundesanstalt für Landtechnik).

#### 2.1 Test setup – measurement methods

**BOILER TEST RIG WITH HEAT EXCHANGER:** Heat output measurement by directly measuring the amount of water circulated through the heating circuit and its temperature increase (DIN 4702-2:1990).

**FLUE GAS EXTRACTION** through a vertical measuring section, generating the feed pressure using a flue pipe, diameter 200 mm, height above ground level 9 m, feed pressure limited by draught limiting flap.

**HEAT OUTPUT MEASUREMENT:** Determining the mass flow using the Coriolis mass flow meter PROMASS 63 F from Endress & Hauser, as well as the water temperatures at the boiler flow/return using a Pt 100 resistance thermometer, 1/3 DIN, calibrated as a pair.

**FLUE GAS TEMPERATURE** in the measuring section using a measurement system with 5 Pt 100 resistance thermometers.

FEED PRESSURE using ring balance.

**WATER-SIDE RESISTANCE:** Differential pressure transducer with ceramic measurement membranes, DELTABAR S PMD 230 from Endress & Hauser.

**CARBON DIOXIDE AND CARBON MONOXIDE CONTENT:** Non-dispersive infrared gas analyser NGA 2000 from Emerson; carbon dioxide: lowest measurement range 0 - 5 %, highest measurement range 0 - 20 %; carbon monoxide: CO Low - lowest measurement range 0 - 50 ppm, highest measurement range 0 - 2500 ppm, CO High - lowest measurement range 0 - 1.0 %, highest measurement range 0 - 10 %; measured in dry flue gas.

**DUST CONTENT:** Dust measurement unit from Ströhlein with a nominal extraction rate of 4 m<sup>3</sup>/h, dust separation on plugged quartz wool filter; filter directly behind the sample probe and angled section, determination of the partial flow using a dry gas meter and upstream drying tower. The sampling point for determining the dust content is immediately after the measuring section.

**CONTENT OF ORGANIC GASEOUS SUBSTANCES:** Flame ionisation detector from JUM, Type VE 5; samples taken via heated filter and heated pipe (thermostatically controlled to 180  $^{\circ}$ C); measured in damp flue gas.

**NITROGEN MONOXIDE CONTENT:** Gas analyser from ECO PHYSICS, Type CLD 700 EI-ht; chemiluminescent measurement principle, samples taken via heated filter and heated pipe; gas cooler; measured in dry flue gas.



**ELECTRICAL POWER CONSUMPTION** Modular energy meter ULYS ETD from ENERDIS, three-phase 100-400 with a measurement accuracy for active energy corresponding to IEC 61036/EN61036 Cl.1. Maximum resolution of the pulse output: 0.1 Wh.

AC power analyser D5155 from NORMA with the following characteristics: measurement of voltage, current, active power, reactive power with a measurement accuracy of +/- 0.1 % of measured value + 0.1 % of full scale for voltage and current and +/- 0.5 % of measurement range for active power.

**DATA LOGGING** using TopMessage data logging system from Delphin Technologie AG, sampling interval 1 second, average value determined from 10 measurements, average data stored to media.

## 2.2 Performance of heating tests

**HEAT OUTPUT:** Measurements were carried out in accordance with ÖNORM EN 303-5:1999 at nominal and minimum heat output respectively (≤ 30 % of the nominal heat output). The nominal heat output measurements were performed after the burner had been operated for at least 3 hours in the nominal heat output range. The measurements themselves were taken over a test period of at least 6 hours. The efficiency was calculated by taking into account the heat stored in the boiler water.

**EMISSIONS:** Carbon dioxide, carbon monoxide, organic carbon and nitrogen oxide values were averaged over the whole test duration. When determining the dust content, the extraction time per filter was limited to 30 minutes. The dust content was determined from 6 half-hourly averages, evenly distributed over the test duration. Calibration gases were used to check the gas analysers before and after every test period.

**SETTINGS:** The declared measurements relate to reproducible tests using optimised settings. The settings were made during preliminary tests based on manufacturer recommendations. The aim was to maximise the carbon dioxide content whilst at the same time minimising the carbon monoxide content.

**FUEL:** The measurements were performed with wood pellets compliant to ÖNORM M 7135:2000, having a diameter of 6 mm and a water content of 6.7 % and 6.6 %. The water content was measured; the average values for the basic chemical data relating to the water and ash-free substances as well as the calorific value were taken from ÖNORM M 7132:1998.

**FUNCTION CHECK** of the temperature controller, safety temperature limiter and monitor as well as a functional check to verify the rapid shutdown of the burner system. The measurements were performed as specified in 5.13 and 5.14 of ÖNORM EN 303-5:1999.

#### 2.3 Interpretation of emission measurements

The emission measurements were analysed by calculating the complete flue gas analysis using the carbon monoxide and carbon dioxide content averaged over the measurement period together with the fuel composition data. The speed of the flue gas at the measuring point was calculated from the flue gas volume and taking into account the pressure and temperature.

The organic gas substances content was measured in the damp flue gas; the emissions were then converted for dry flue gas conditions and declared as organic carbon. The nitrogen oxide content was measured in the dry flue gas and declared as NO<sub>2</sub>.



# 2.4 Investigatory heating tests with wood pellets at nominal heat output

Test name	Nominal	heat outp	ut	
Number of test: Name of boiler: Nominal heat output:	HKA_1217 Pellet burner PELLEMATIC PE32 32 kW			E32
		Minimum value	_	Maximum value
Test conditions				
Start of test: End of test: Test duration:			5-01-10 1 5-01-10 1 06:03	
Ambient temperature: Outside temperature: Air pressure:	°C °C mbar	17.9 2.1	20.8 5.8 1003	26.8 7.2
Test fuel, heat input				
Test fuel Water content Ash content Carbon content Hydrogen content Oxygen content	Wood pe kg/kg kg/kg kg/kg kg/kg kg/kg	llets	0.067 0.002 0.473 0.058 0.400	
Calorific value of anhydrous and ash-free substance Calorific value of test fuel	MJ/kg MJ/kg		19.0 17.5	
Applied fuel quantity Hourly fuel quantity Fuel heat input	kg kg/h kW		43.4 7.2 34.9	
Heat output, efficiency				
Water circulation Flow temperature Return temperature Temperature difference	kg/h °C °C K	1364.5 51.8 71.6 19.1	1371.4 52.7 72.6 20.0	1377.6 53.2 73.5 20.7
Heat output in the boiler circuit Utilisation Boiler efficiency	kW % %		31.9 99.7 91.4	
Measured values flue gas measur	ing sect	ion		
Flue gas temperature Manometric pressure (draught)	°C Pa	129.6 12.2	130.9 13.3	131.8 15.9
Carbon dioxide Carbon monoxide Organic gaseous substances Nitrogen monoxide	% ppm ppm	11.0 15.5 0.0 80.8	13.2 36.6 0.0 98.2	15.5 144.3 1.7 115.5



### 2.4.1 Emission measurements

## Measurement results test: HKA\_1217

(Calculation depending on CO<sub>2</sub>-measurement)

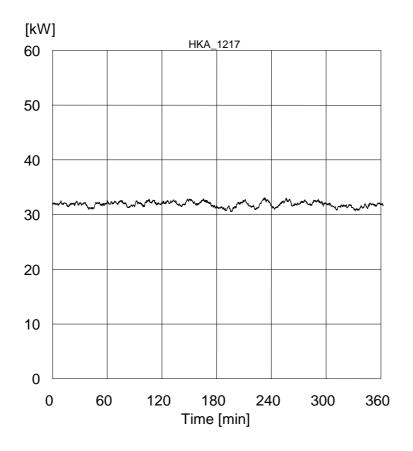
Suction start:	hh:mm	10:10	11:10	12:10	13:10	14:10	15:10
Suction period:	min	30	30	30	30	30	30
Measured $CO_2$ -content: Calculated $O_2$ -content:	olo olo	13.2 7.2	13.2 7.2	13.4 7.1	13.2 7.3	13.5 7.0	13.0 7.5
Density of gas sample Dry gas Humid gas Water content	kg/Nm <sup>3</sup> kg/Nm <sup>3</sup> g/Nm <sup>3</sup>	1.36 1.30 78.9	1.36 1.30 78.8	1.36 1.30 79.5	1.36 1.30 78.5	1.36 1.30 80.2	1.36 1.30 77.3
Velocity: at sampling point at probe head	m/s m/s	1.25 1.05	1.25 1.01	1.24	1.25 1.08	1.22 1.18	1.27 1.22
Dust content: separated	mg	12.7	11.8	12.1	12.3	11.9	12.3
Spec. dust content	$mg/Nm^3$	22.7	21.9	21.4	21.4	18.9	18.8

## 2.4.2 Evaluation

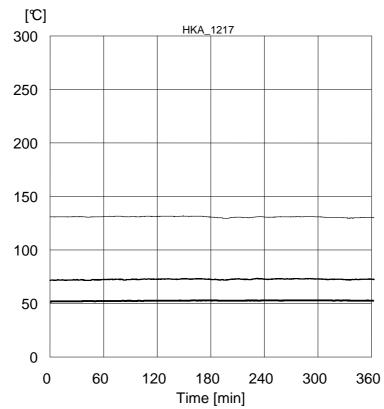
	relating to plied energy	relati O <sub>2</sub> -cont	_
	mg/MJ	10 % mg/Nm³	$13 \% $ mg/Nm $^3$
Dust	8	17	12
Carbon monoxide (CO)	17	37	27
Organic gaseous substances(OGC)	<1	<1	<1
Nitrogen oxides $(NO_x)$	77	162	117



# 2.4.3 Output-related measurements



Heat output

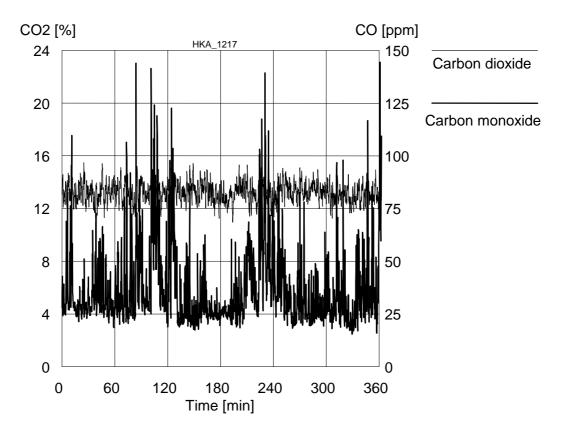


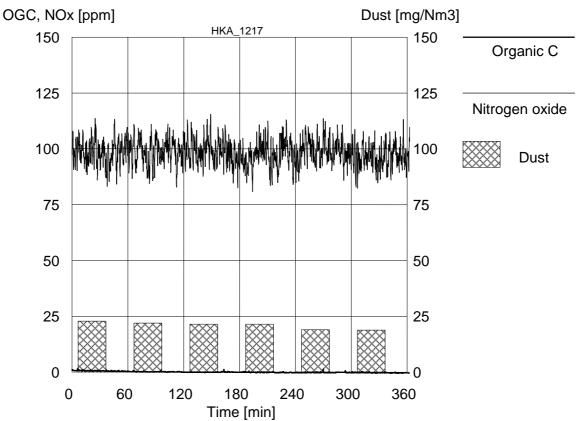
Flue gas temp.

Flow temp.

Return temp.

## 2.4.4 Flue gas composition





# 2.5 Investigatory heating tests with wood pellets at minimum heat output

Test name	Minimum	heat outpo	ut	
Number of test: Name of boiler: Nominal heat output:	HKA_121 Pellet 1 32 kW	8 burner PEL1	LEMATIC PE	32
		Minimum value	Average value	Maximum value
Test conditions				
Start of test: End of test: Test duration:			5-01-11 10 5-01-11 16 06:07	
Ambient temperature: Outside temperature: Air pressure:	°C °C mbar	19.5 0.6	21.3 5.7 1004	26.9 8.1
Test fuel, heat input				
Test fuel Water content Ash content Carbon content Hydrogen content Oxygen content	Wood pe kg/kg kg/kg kg/kg kg/kg kg/kg	llets	0.066 0.002 0.473 0.058 0.401	
Calorific value of anhydrous and ash-free substance Calorific value of fuel	MJ/kg MJ/kg		19.0 17.5	
Applied fuel quantity Hourly fuel quantity Fuel heat input	kg kg/h kW		12.2 2.0 9.7	
Heat output, efficiency				
Water circulation Flow temperature Return temperature Temperature difference	kg/h °C °C K	408.1 52.1 70.6 18.1	411.4 52.8 71.4 18.6	414.1 53.6 73.3 20.0
Heat output in the boiler circuit Utilisation Boiler efficiency	kW % %		8.9 27.7 91.2	
Measured values flue gas measur	ing sect	ion		
Flue gas temperature Manometric pressure (draught)	°C Pa	79.8 7.2	80.8	83.1 11.0
Carbon dioxide Carbon monoxide Organic gaseous substances Nitrogen monoxide	% ppm ppm	8.7 52.7 0.8 52.6	10.0 110.5 1.0 60.5	11.2 283.5 1.7 67.7



### 2.5.1 Emission measurements

## Measurement results test: HKA\_1218

(Calculation depending on CO<sub>2</sub>-measurement)

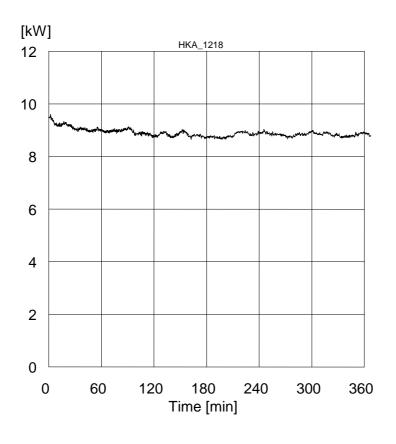
Suction start:	hh:mm	10:05	11:05	12:05	13:05	14:05	15:05
Suction period:	min	30	30	30	30	30	30
Measured CO <sub>2</sub> -content: Calculated O <sub>2</sub> -content:	00 00	10.0 10.6	10.2 10.4	10.1 10.5	10.0 10.6	10.0 10.6	10.1 10.5
Density of Gas sample Dry gas Humid gas Water content	kg/Nm³ kg/Nm³ g/Nm³	1.34 1.30 60.8	1.34 1.30 62.1	1.34 1.30 61.5	1.34 1.30 61.1	1.34 1.30 60.8	1.34 1.30 61.7
Velocity: at sampling point at probe head	m/s m/s	0.40	0.39	0.39	0.39	0.39	0.39 0.67
Dust content: separated	mg	27.8	24.2	30.5	27.4	23.3	23.2
Spec. dust content	${\rm mg/Nm^3}$	51.0	40.4	54.1	48.2	39.0	38.7

#### 2.5.2 Evaluation

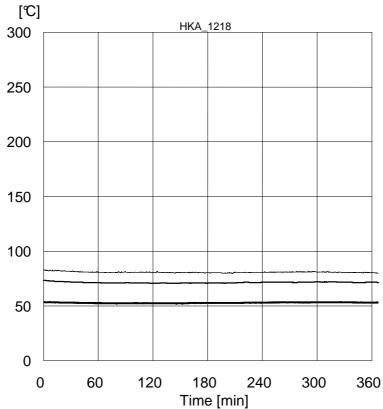
	relating to applied energy		ing to ent of
	mg/MJ	10 % mg/Nm³	13 % mg/Nm³
Dust	23	48	35
Carbon monoxide (CO)	69	146	106
Organic gaseous substances (O	GC) <1	2	1
Nitrogen oxides $(NO_x)$	62	131	96



# 2.5.3 Output-related measurements



Heat output

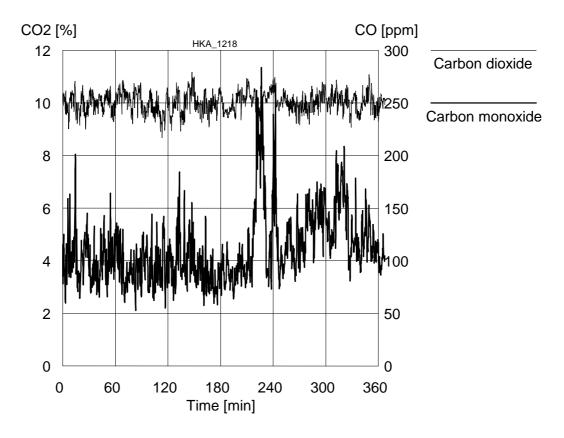


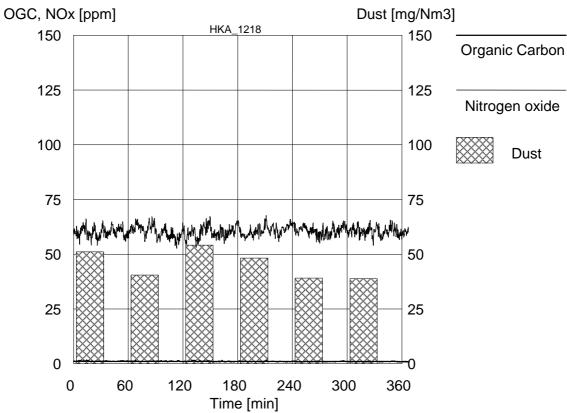
Flue gas temp.

Flow temp.

Return temp.

# 2.5.4 Flue gas composition





#### 2.6 Surface losses

The heat loss through the boiler surface is determined using DIN 4702-2:1990 based on radiation coefficients and arrangements of technical surfaces (according to Nusselt). Temperatures were measured at 47 points on the boiler surface during the test at nominal heat output. The measurement results are shown in the following table and the table of measurements in appendix 5.2:

Parameter	Value	Unit
Test number	HKA_1217	
Ambient temperature	23	Ç
Flow temperature	73	Ĉ
Flue gas temperature	131	S
Heat output in the boiler circuit	31.9	kW
Radiation losses from boiler	0.22	kW
Percentage loss at nominal heat output	0.7	%

The surface temperature of the handle on the combustion chamber/ash door is 1 K above the ambient temperature.

#### 2.7 Water-side resistance of boiler

The water-side resistance was determined for the flow rates at nominal heat output which occurred at temperature differences of 10 K and 20 K.

Flow rate	Temperature difference	Water temperature	Differential pressure
[kg/h]	[K]	[°]	[mbar]
1370	20	21.8	95.4
1370	10	21.9	376.4

## 2.8 Electrical power consumption

# 2.8.1 Average electrical power consumption at nominal heat output, minimum heat output, during standby position and ignition

Operating status	Fuel	Meas. duration	Electrical energy	Average electrical power consumption	Percentage of nominal heat output		
		[min]	[Wh]	[W]	[%]		
Nominal heat output	Wood polloto	363	867	143	0.4		
Minimum heat output		448	329	44	0.1		
Standby position	Wood pellets	60	11.6	11.6			
Ignition procedure		15.7	98	374			

# 2.8.2 Electrical power consumption of main loads

Load	Power [W]
Drive motor – stoker screw	21
Drive motor – extraction screw	49
Induced draught fan	27
Combustion fan (primary/secondary air)	61
Ignition rod	255
Heat exchanger cleaning motor	39



#### 3 SUMMARY OF RESULTS

### 3.1 Heating tests

The PELLEMATIC PE32 pellet burner from ÖkoFEN Forschungs- und Entwicklungs Ges.m.b.H. with a nominal heat output of 32.0 kW, was tested in the power range 8.9 kW - 31.9 kW using wood pellets compliant to ÖNORM M 7135:2000 having a diameter of 6 mm and a water content of 6.7 % and 6.6 %.

Since the boiler flue gas temperature is less than 160 K above room temperature at nominal heat output, the boiler manufacturer shall make recommendations, in accordance with ÖNORM EN 303-5:1999, regarding the flue installation in order to ensure sufficient draught and to prevent sooting up of the chimney and condensation.

The results of the emission measurements are as follows:

		Nom	inal heat or	utput	Minimum heat output:					
Test fuel	[-]		Wood pellets							
Water content	[%]		6.7		6.6					
Heat output	[kW]		31.9			8.9				
Load	[%]		99.7		27.7					
Flue gas temperature	[C]		130.9		80.8					
Boiler efficiency	[%]		91.4		91.2					
Carbon dioxide	[%]		13.2		10.0					
		[mg/MJ] 1)	[mg/m <sup>3</sup> ] <sup>2)</sup>	[mg/m <sup>3</sup> ] <sup>3)</sup>	[mg/MJ] 1)	[mg/m <sup>3</sup> ] <sup>2)</sup>	[mg/m <sup>3</sup> ] <sup>3)</sup>			
Dust		8	17	12 <b>23</b>		48	35			
Carbon monoxide		17	37	27	69	146	106			
Organic carbon		<1	<1	<1	<1 <b>&lt;1</b>		1			
Nitrogen oxides		77	162	117	62	131	96			

- 1) Emission values in mg/MJ (relating to the applied energy), subject to legal requirements in Austria.
- 2) Emission values in mg/m³ (relating to 10 % O<sub>2</sub>, 1013 mbar, dry flue gas), corresponding to ÖNORM EN 303-5:1999.
- 3) Emission values in  $mg/m^3$  (relating to 13 %  $O_2$ , 1013 mbar, dry flue gas), corresponding to various domestic and international requirements.



# 3.2 Function check of the temperature controller / safety temperature limiter on the boiler

The functional check of the temperature controller and safety temperature limiter and monitor on the boiler was performed in accordance with section 5.13 of ÖNORM EN 303-5. The requirements were fulfilled.

#### 3.3 Function check to verify the rapid shutdown of the burner system

Since the tested PELLEMATIC PE32 pellet burner from ÖkoFEN Forschungs- und Entwicklungs Ges.m.b.H. is not equipped with a device to dissipate the residual heat as described in section 4.1.5.11.3 of ÖNORM EN 303-5, the operating and fault conditions associated with a power outage and sudden loss of heat extraction were simulated to satisfy the definition of a burner system with a rapid shutdown facility.

No dangerous operating conditions arose with either the water system or the burner during the course of the checks on the temperature controller, safety temperature limiter and rapid shutdown facility.

#### 4 ASSESSMENT

Based on the test results, one can hereby confirm that the

Pellet burner PELLEMATIC PE32
from
ÖkoFEN Forschungs- und Entwicklungs Ges.m.b.H.,

fulfils the requirements governed by the agreements in Art. 15 a BV-G relating to "Protective measures for small burners" (1998) and "Saving energy" (1995).

For the For the factual correctness: report and tests:

Amtsdirektor Dipl.-HLFL-Ing. Leopold Lasselsberger m.p.

Ing. Harald Baumgartner m.p.

Head of the accredited test centre:

Hofrat Dipl.-Ing. Dr. Johann Schrottmaier m.p.

Wieselburg, 27/04/05



#### 5 APPENDIX

## 5.1 Legal requirements (for information only)

# Legal requirements relating to small burner systems for biogenous fuels in Austria

Agreement according to Art. 15 a B-VG concerning an amendment to the agreement according to Art. 15 a B-VG relating to protective measures for small burners (1998)

Small solid fuel burners should not exceed the following emission limits:

Solid	fuel burners	Emission limits [mg/MJ]								
Solid	ruei burriers	СО	NO <sub>x</sub>	OGC	Dust					
Manually loaded	Biogenous fuels	1100	150*)	80	60					
	Fossil fuels	1100	100	80	60					
Automatically loaded	Biogenous fuels	500**)	150*)	40	60					
	Fossil fuels	500	100	40	40					

<sup>\*)</sup> The NOx limit only applies to wood burners.

Energy saving agreement according to Art. 15 a B-VG

The efficiency of small solid fuel burners should not fall below the following values:

Small burners used for solid fuel central heating:									
Manually loaded									
up to 10 kW	73 %								
> 10 to 200 kW	(65.3 + 7.7 log Pn) %								
> 200 kW	83 %								
Automatically loaded									
up to 10 kW	76 %								
> 10 to 200 kW	(68.3 + 7.7 log Pn) %								
> 200 kW	86 %								

These federal requirements are implemented in local state law.



<sup>\*\*)</sup> This limit value can be exceeded by 50 % during partial load operation at 30 % of nominal output.

# 5.2 Surface temperature measurement points

KESSELFABRIKAT: Ökofen Forschungs- u. EntwicklungsGmbH KESSELTYPE: Pelletskessel PE												essel PE32					
M	MESSPUNKT POSITIONSBESCHREIBUNG			MATERIAL TEMP. MESSPUNKT			ESSPUNKT	POSITIONSBESCHREIBUNG					ERIAL	TEMP.			
	BEZ. DES BEDIENUNGSGRIFFES		(ME / PO / KU)		[%]		BEZ.	DES BEDIENUNGSGRIFFES				(ME	/ PO / KU)	[3]			
	Z1	Gı	riff -	Brennraumt	ür		ME	24	Z3								
	Z2									Z4							
MESS TEMP. MESS TEMP.		MESS.		TEMP	TEMP. MESS		TEMP. MESS TEMP.			TEMP	MESS		TEMP.				
NR.	FLÄCHE		NR.	FLÄCHE		NR.	FLÄCHE		NR.	FLÄCH E	[°C]	NR.	FLÄCHE	[°C]	NR.	FLÄCHE	[°C]
1	A1	30.7	21	E1	28.7	41	11	, ,,	61	M1	( -)	61	Q1		61	U1	
2	A2	31,0	22	E2	28,4	42	12		62	M2		62	Q2		62	U2	
3	A3	31,3	23	E3	29,6	43	13		63	M3		63	Q3		63	U3	
4	A4	,	24	E4	28,4	44	14		64	M4		64	Q4		64	U4	
5	A5		25	E5	28,8	45	15		65	M5		65	Q5		65	U5	
	Mittelwert	31,0		Mittelwert	28,8		Mittelwert			Mittelwert			Mittelwert			Mittelwert	
6	B1	28,7	26	F1	27,6	46	J1	28,8	66	N1		66	R1		66	V1	
7	B2	29,6	27	F2	28,7	47	J2	27,0	67	N2		67	R2		67	V2	
8	B3	29,5	28	F3	25,5	48	J3	29,6	68	N3		68	R3		68	V3	
9	B4	29,5	29	F4	25,8	49	J4	31,6	69	N4		69	R4		69	V4	
10	B5	31,7	30	F5		50	J5	28,5	70	N5		70	R5		70	V5	
	Mittelwert	29,8		Mittelwert	26,9		Mittelwert	29,1		Mittelwert			Mittelwert			Mittelwert	
11	C1	32,1	31	G1	27,3	51	K1	29,9	71	01		71	S1		71	W1	
12	C2	34,8	32	G2	28,2	52	K2	29,8	72	02		72	S2		72	W2	
13	C3	28,7	33	G3	26,2	53	K3	38,9	73	O3		73	S3		73	W3	
14	C4	29,7	34	G4	27,3	54	K4	29,1	74	04		74	S4		74	W4	
15	C5	30,3	35	G5	25,4	55	K5	29,3	75	O5		75	S5		75	W5	
	Mittelwert	31,1		Mittelwert	26,9		Mittelwert	31,4		Mittelwert			Mittelwert			Mittelwert	
16	D1	26,8	36	H1	40,2	56	L1		76	P1		76	T1		76	X1	
17	D2	26,9	37	H2	35,2	57	L2		77	P2		77	T2		77	X2	
18	D3	31,6	38	H3	24,8	58	L3		78	P3		78	T3		78	Х3	
19	D4	27,2	39	H4	24,3	59	L4		79	P4		79	T4		79	X4	
20	D5	27,9	40	H5	24,4	60	L5		80	P5		80	T5		80	X5	
	Mittelwert	28,1		Mittelwert	29,8		Mittelwert			Mittelwert			Mittelwert			Mittelwert	

K1...K5 Floor area