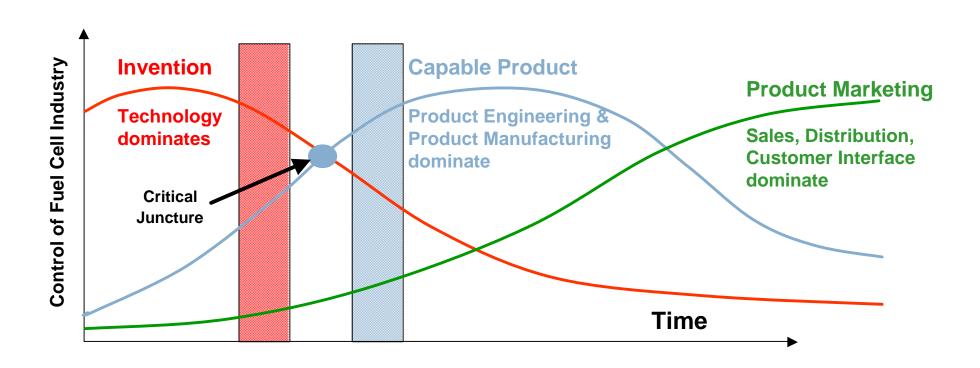
General Motors Fuel Cell Research



Andrew Bosco
Manager Fuel Cell Stack Research



Fuel cell industry entering a transition phase in which engineering and manufacturing will become as important as technical leadership





Fuel Cell Activities Formed in 1997 Stack Research Locations

Warren (MI, USA):

Bipolar Plate & Catalyst Diagnostics, Modeling

Honeoye Falls (NY, USA):

Stack Design, MEA, DM, Catalyst,

Diagnostics, Modeling, Freeze

Mainz-Kastel (Germany):

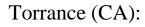
Stack/Vehicle Integration,

Material Development, Modeling







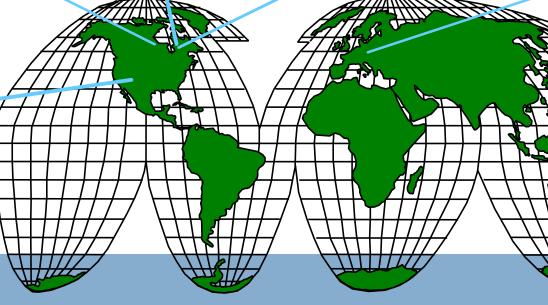


Stack/Electronics

Interface











Fuel Cell Propulsion System



Fuel Cell Propulsion System (FCPS)

Vehicle Connections, Controls, Thermal Integration:

Fuel Storage $(H_2 \text{ on board} \rightarrow H_2 \text{ to FCPM})$ Fuel Cell Power Module (FCPM) $(H_2 \text{ in} \rightarrow DC \text{ electrical power out})$

Traction (DC in \rightarrow Torque out)

Liquid



Compressed

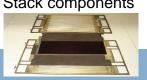




Stack



Stack components



FCPM Subsystems





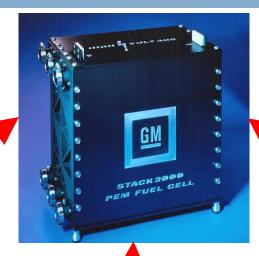








Automotive Stack Research



Cost

- Stack:
 - Material
 - Processing
 - Assembly
- Low Pressure
- Humidifiaction
- Passive Anode Control

Life

- Durability
- Start/Stops
- Degradation
- Coolant Compatibility

Performance

- Volumetric Power Density
- Gravimetric Power Density
- Transients
- Freeze Capable
- High Temperature

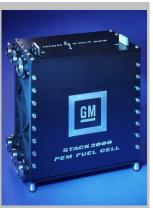


Fuel Cell Stack Technology Progress











St 3 - 1997

St 4 - 1998

St 7 - 1999

Stack 2000

Current

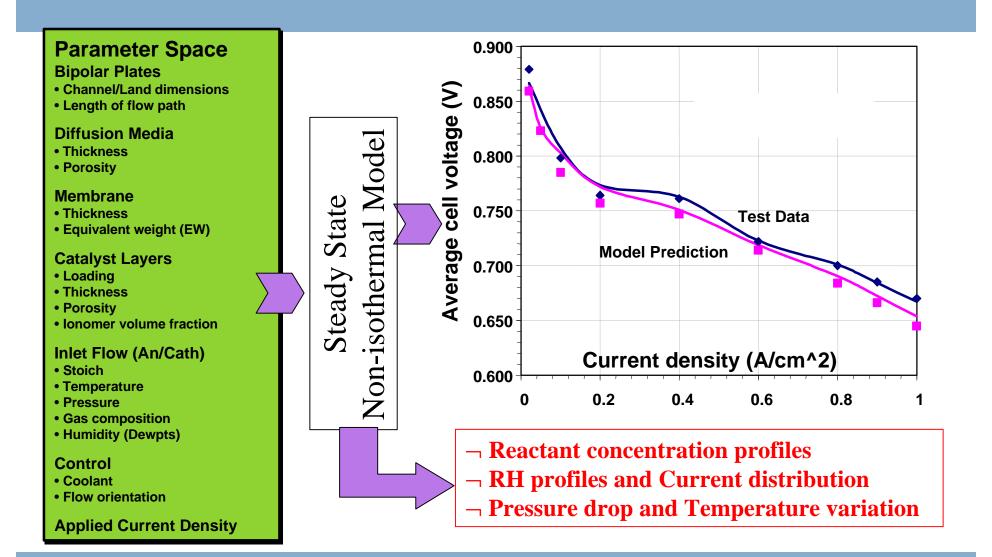
Max. Power: 37-41 kW 40 kW 50 - 120 kW 80 - 120 kW 102 kW Power density: 0.26 kW/l 0.77 kW/l 1.10 kW/l 1.44 kW/l 1.75 kW/l 0.31 kW/kg 0.16 kW/kg 0.47 kW/kg 0.83 kW/kg 1.25 kW/kg 500 cm² 500 cm² 800 cm² 800 cm^2 250 cm² Active area:

Pressure: 2.7 bar 2.7 bar 2.7 bar 1.5 - 2.7 bar 1.2-1.5 bar

Temperature: 80 °C 80 °C 80 °C 80 °C 80 °C



Electrochemical Stack Model





Stack Research Driven by System Interactions & Requirements

"Device"	1 1	- 3	2 3	4	5	1 6	7	8	0	10	11	12	12	14	15	16	17	10	10	20	21	22	22	24	25	26	27	28	20	30	21	32	
Anode side pressure system	x	x	_		_	+ -	+-	x	- 9	10	-11	-12	13	-14	_10	x		10	19	X	X X	22	23	24	20	20	23	:20	29	- 20	91	32	-
Anode side temperature system	x	0	_	_	X	-	+	X	-	-	-	\vdash	\rightarrow	-		x	×.	-	_	x	х	х	-	-		-	-		-	÷ :	_	-	
Anode side humidification system	x	x		_		-	+-	-	\vdash	-			\rightarrow	-	x	x		x	-	X	-	x	-	-		_	-		-	-	_		_
Anode side flow control	×	x	_			-	1				-				_x_	x		X	-	X	x	x	-	-	-		-		-	-		-	
Cathode pressure control system	x	X	X	0	0	x	x	x	x	х	x		-	5-5	_	x	х			X	x	×	-							9 0		3 - 1,	
Cathode pressure control system Cathode humidification System	- ^	-		1	х	0	x	x	x	X	X				x	х	x		x	, A	x	x											
Cathode from Cathode temperature System	_			-	x	x	0	x	x	X	x						x		X		x	x										7	
Cathode pressurization system	x		1	-	x	x	x	0	x	x	x				_	x	x	\vdash	_	x	x	X				_	_		_				-
Cathode flow control system Cathode flow control system	_ X	-	+	-	x	X	x	x	0	x	x		-		_	X	x			x	x		-	-	-					-		-	
Uster vapor recovery system	-	-	+	-	x	x	x	x	x	0	x		-		×	-	x	_	х	x	x	х	-	-		_	-		-	9-1	_	-	_
1 Liquid water recovery system		-	+	-	x	x	x	x	x	x	0		-	-	x x	-	x		x		x	x		-		_	_		-	-	_		_
2 Water Cleaning system		-	+	1	х	X	X	X	X	X	0	0	-	-	_x_	-	X		X	х	x	x	x	-	x		-		-	-	_	-	
Water Clearing system Heat Rejection system (temperature sink)	-		1	-		100		1 1				0	8	765	*	- 0				Х	х	X	X	-	х					0 0			
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COOLANT FLOWFIELD	-		x		1	-	1			_			X)	0	_ <u>X</u>	х	x						<u> </u>	х	Х	x							
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	X	100	48	х	х	x	X	X	х	X	X	х		-		2 2			X	24	0	X	100	20-15 20-12	x	х				100			
MEMBRANE	2250	X	X	_ X_		X	<u> x</u>			X	X	Х	-		_x_					<u> x</u>	<u>x</u> .	0	х	х	х	х							
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PLATE COATING		-		_	1				_	_		х		X		_				х	х	х	х	х	0	Х	_						
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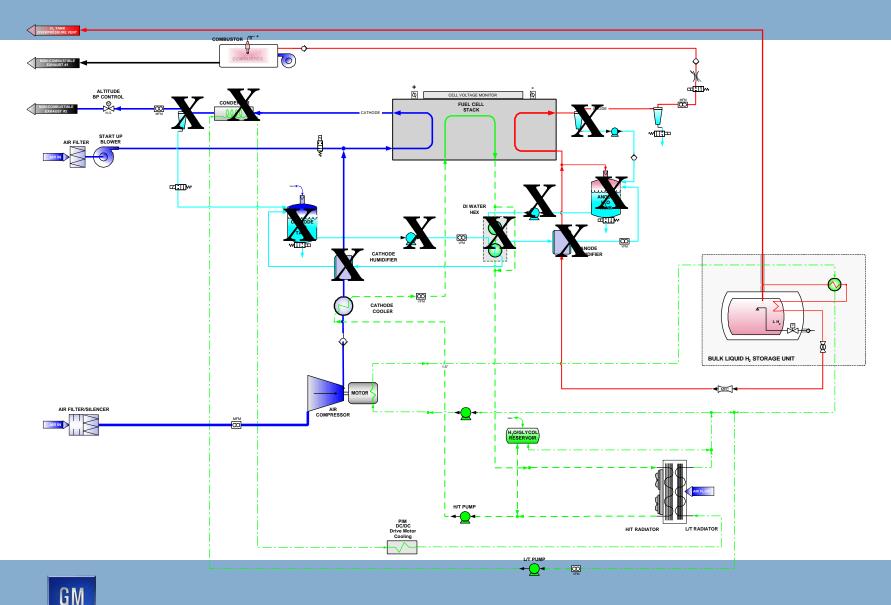


System & Stack Trade-offs

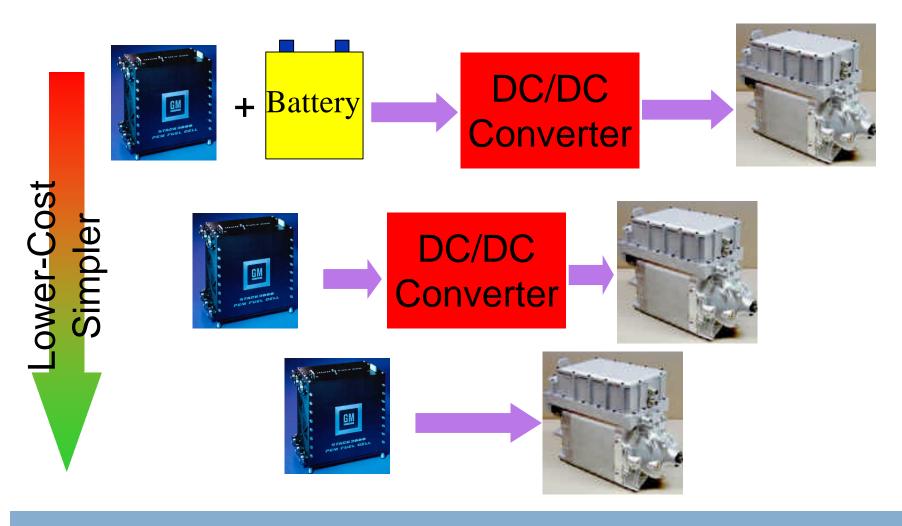
	in	npact on	system	requ'm	ent
	weight	volume	complexity	system	stack
Operating pressure	X	X	X	low	high
Operating temperature	X	X		high	med
Reactant stoichiometry	X	X	X	low	high
Inlet Relative Humidity	X	X	X	low	high
Stack weight	X			low	low
Stack volume		X		low	low
Stack voltage			X	high	low
Stack Efficiency (cell voltage)	Χ	Х		high	high
Durability				high	high
Start time @ freezing temps			X	low	low
Cost				low	low



System Simplification – No External RH



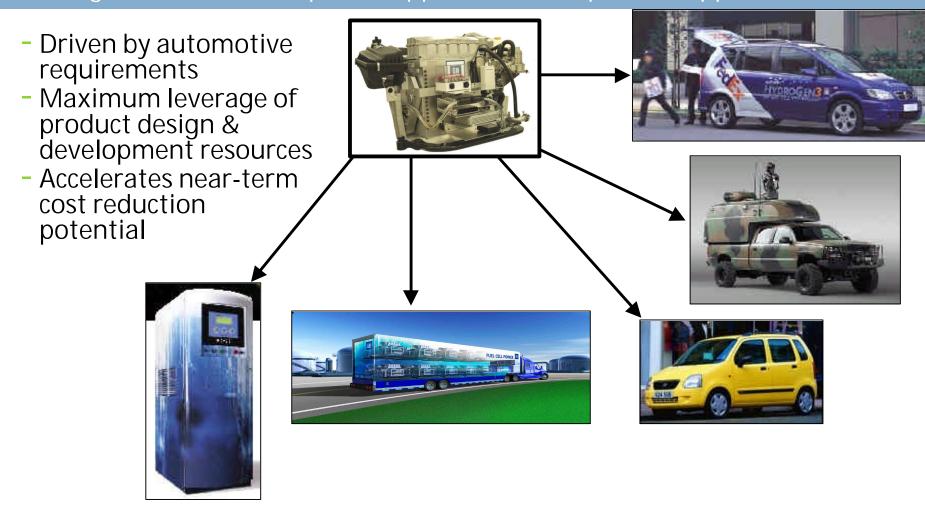
System Simplification - Power Management





Engineering Focus

Single module development approach across product applications





End users requirements have outgrown current technology solutions



Gas Turbines

Very difficult to site



Reciprocating Generators

Noisy and dirty



Uninterruptible Power Supplies

Battery failures and expensive

Fuel Cell solutions exploit vulnerabilities of existing technologies

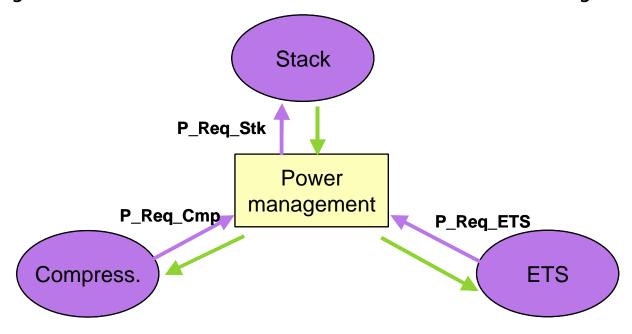






Interactions

Key interfaces that exist in Fuel Cell Systems



 Batteries and Fuel Cell Stacks have different voltage characteristics



DC Source Resistance

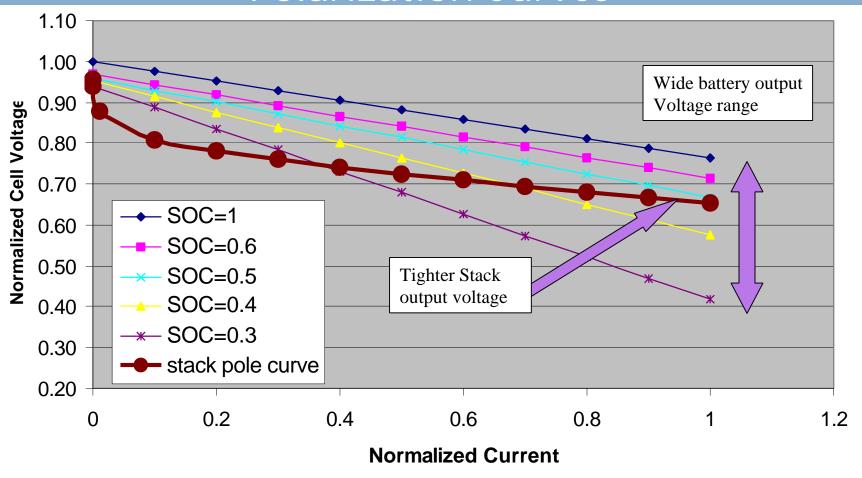
	DC Resistance							
В	attery	Fuel Cell Stack						
soc	Resistance (Ohms)	Resistance (Ohms)						
0	0.789	0.160						
0.1	0.718							
0.2	0.656							
0.3	0.522							
0.4	0.374							
0.5	0.293							
0.6	0.254							
0.7	0.239							
0.8	0.227							
0.9	0.229							
1	0.237							

- •The DC source resistance for a battery is dependant on it's State of charge
- Stack Resistance is constant, and is dependent on materials development



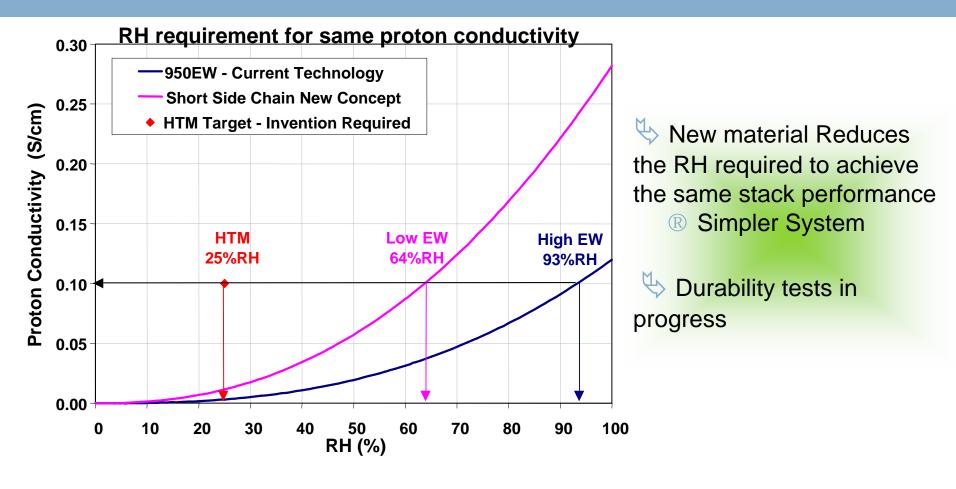
Comparing Stack and Battery

"Polarization Curves"





Material & System design can impact fuel cell stack resistance





Voltages

Voltages											
	Battery	Fuel Cell Stack									
SOC	Open Circuit	Full Load	Open Circuit	Full Load							
100%	1.00	0.76	1.00	0.65							
30%	0.93	0.42									

- •The output voltage for a battery will depend on its state of charge.
- •At full load the battery output voltage as function of SOC can vary as much 55%
- •Battery full load voltage is 64% lower than that of a stack



Summary

- General Motors Research is Focused on Fundamental Material & Design Development
- Traction System, Power Conditioning & Stack Development Required to meet Automotive Targets





